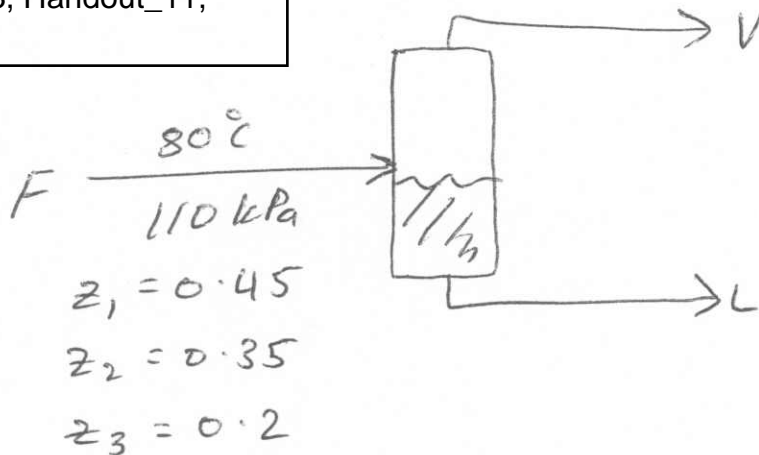


Example 70.5 The system acetone(1)/acetonitrile(2)/nitromethane(3) at 80°C and 110 kPa has the overall composition, $z_1 = 0.45$, $z_2 = 0.35$, $z_3 = 0.20$. Assuming that Raoult's law is appropriate to this system, determine \mathcal{L} , \mathcal{V} , $\{x_i\}$, and $\{y_i\}$.

The vapor pressures of the pure species at 80°C are

$$P_1^{\text{sat}} = 195.75 \quad P_2^{\text{sat}} = 97.84 \quad P_3^{\text{sat}} = 50.32 \text{ kPa}$$

Chemical Engineering Dept.,
KFUPM, CHE303, Handout_11,
Flash



First make sure that the feed is a two phase system. To do that, check:

$$P_{\text{dew}} < P = 110 \text{ kPa} < P_{\text{bubl}}$$

Raoult's law: $y_i P = x_i P_i^{\text{sat}}$

BUBL P: $\sum y_i = 1 \Rightarrow P_{\text{bubl}} = \sum_{i=1}^N x_i P_i^{\text{sat}}$

replace $x_i = z_i$

$$P_{\text{bubl}} = (0.45)(195.75) + (0.35)(97.84) + (0.2)(50.32) = 132.4 \text{ kPa}$$

DEW P: $\sum x_i = 1 \Rightarrow P_{\text{dew}} = \frac{1}{\sum_{i=1}^N \frac{y_i}{P_i^{\text{sat}}}}$

replace $y_i = z_i$

$$P_{dew} = \frac{0.45}{195.75} + \frac{0.35}{97.84} + \frac{0.20}{50.32}$$
$$= 101.52 \text{ kPa}$$

In deed $P_{dew} < P < P_{bubble} \Rightarrow$ Two phase system.

Since P and T are known

$$\sum_{i=1}^N \frac{z_i k_i}{1 + V(k_i - 1)} = 1 \leftarrow \begin{matrix} \text{basis} \\ F = 1 \text{ mole/s} \end{matrix}$$

$$k_i = \frac{P_i^{sat}}{P} \quad (\text{Raoult's Law})$$

$$\Rightarrow k_1 = 1.7795, \quad k_2 = 0.8895, \quad k_3 = 0.4575$$

substitute in the above equation

$$\Rightarrow \frac{(0.45)(1.7795)}{1 + 0.7795V} + \frac{(0.35)(0.8895)}{1 - 0.1105V} + \frac{(0.20)(0.4575)}{1 - 0.5425V} = 1$$

by trial and error $V = 0.7364 \text{ mole/s}$

$$\Rightarrow L = 0.2636 \text{ mole/s}$$

now $y_i = \frac{z_i k_i}{1 + V(k_i - 1)} \quad (i = 1, 2, \dots, N)$ ③

$$\Rightarrow y_1 = 0.5087, \quad y_2 = 0.3389 \quad \& \quad y_3 = 0.1524$$

$$x_i = y_i / k_i$$

$$\Rightarrow x_1 = 0.2859, \quad x_2 = 0.3810 \quad \& \quad x_3 = 0.3331$$

A 3.5 mole/s binary mixture of acetone(1)/methanol(2) contains 25-mole% acetone is flashed at 60 °C. The composition of the liquid leaving the drum contains 17.5-mole% acetone. Assuming that Raoult's is an adequate description for the VLE of this system, calculate:

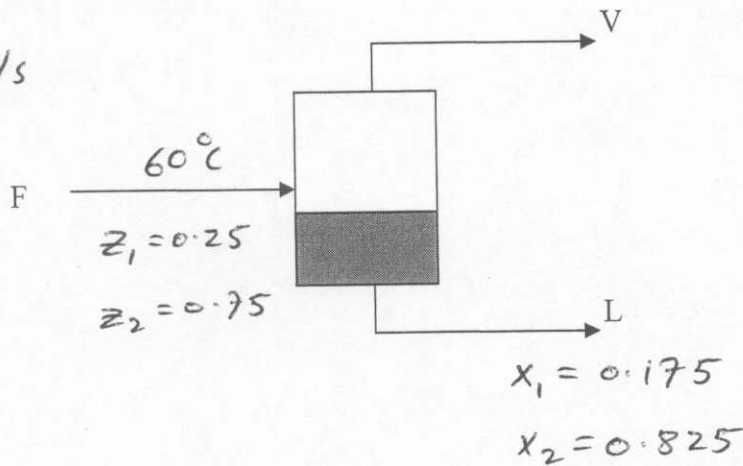
- The pressure of the flash drum.
- The flow rates of the vapor and liquid streams leaving the drum.
- The composition of the vapor stream.

Table 10.2

$$P_1^{\text{sat}} = 115.68 \text{ kPa}$$

$$P_2^{\text{sat}} = 84.47 \text{ kPa}$$

basis $F = 1 \text{ mole/s}$



$$\sum_{i=1}^N \frac{z_i k_i}{1 + V(k_i - 1)} = 1 \quad \text{--- (10.17)}$$

Since P is unknown, $k_i = \frac{P_i^{\text{sat}}}{P}$ also unknown

\Rightarrow the above equation has two unknowns

V and P . \Rightarrow we need one more equation

$$y_i = \frac{z_i k_i}{1 + V(k_i - 1)} \quad (i = 1, 2, \dots, N) \quad (10.16)$$

\uparrow
Unknown

$$y_i = k_i x_i$$

$$\Rightarrow x_i = \frac{z_i}{1 + V(k_i - 1)}, \quad (i = 1, \dots, N) \quad (10.16 \text{ modified})$$

now, we have two equations 10.17 & 10.16 modified with two unknowns V & P .

for $i=1$, solve for V from (10.16 modified) (5)

$$0.175 = \frac{0.25}{1 + V \left(\frac{115.68}{P} - 1 \right)}$$

$$\Rightarrow V = \frac{\frac{0.25}{0.175} - 1}{\frac{115.68}{P} - 1} = \frac{1.429P - P}{115.68 - P} \quad \dots (*)$$

substitute in (10.17)

$$\frac{(0.25) \frac{115.68}{P}}{1 + \frac{(1.429P - P)}{(115.68 - P)} \left(\frac{115.68}{P} - 1 \right)} + \frac{(0.75) \frac{84.47}{P}}{1 + \frac{(1.429P - P)}{(115.68 - P)} \left(\frac{84.47}{P} - 1 \right)} - 1 = 0$$

simplify,

$$\frac{28.92}{1 + \frac{0.429}{(115.68 - P)} (115.68 - P)} + \frac{63.35}{1 + \frac{0.429}{(115.68 - P)} (84.47 - P)} - P = 0$$

$$\Rightarrow \frac{63.35}{1 + \frac{0.429}{(115.68 - P)} (84.47 - P)} - P + 20.238 = 0$$

$P \approx 90$ kPa by trial and error

$$\Rightarrow \text{from } (*) \quad V = 0.017 \frac{\text{mol}}{\text{s}} \Rightarrow L = 1 - V = 0.983$$

note $L \neq V$ where calculated based on
on $F = 1 \text{ mole/s}$. But $F = 3.5 \frac{\text{mol}}{\text{s}}$

$$\Rightarrow V = (3.5)(0.017) = 0.058 \text{ mole/s}$$

$$L = 3.442 \text{ mol/s}$$

$$y_i = \frac{z_i k_i}{1 + V(k_i - 1)}$$

↑
(based on $F = 1 \frac{\text{mol}}{\text{s}}$)

$$\Rightarrow y_1 = \frac{0.25 \frac{115.68}{90}}{1 + 0.017 \left(\frac{115.68}{90} - 1 \right)}$$

$$= 0.32 \quad \Rightarrow y_2 = 0.68$$