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ABSTRACT

The bibliographical study made on thermal conversion solar energy shows that the plane collectors require a vacuum operation to be able to boil water at temperatures which, in general, do not exceed 80 °C and which they are adequate for the heating of the fluids. To cure these disadvantages, one can use the solar concentrators cylindro-parabolic type which can reach temperatures about 300°C. These concentrators can boil brackish water with pressures equal to or higher than the atmospheric pressure and have an output higher than that of the plane collectors. By working out simulation and calculation programmes, we could determine dimensions of the various elements of a unit of desalination of brackish water. The results obtained show that the use of a cylindro-parabolic concentrator of diameter of collecting apparent equal to one meter and an absorbent tube of diameter equal to 0.01m working with high report/ratio of concentration can

produce nearly seven liters of water distilled per day per m² according to the density of the average solar flow of the area. The economic feasibility study shows that the realization of a unit of 30 m² surface of collecting is possible and has an acceptable index of profitability. Considering these results encouraging, we are spirit to carry out an experimental unit in order to check and compare the various results.

[Clerfayt, A., 1967]

[Vaillant, J.R., 1978]

{ }

[Desautel, J., 1979 Bernard, R. et al., 1980]

:

$$P_a = P_u + P_e$$

: (Pa)

$$P_a = E \cdot \rho \cdot C \cdot \tau \cdot \alpha$$

:

$$P_u = q \cdot C \cdot (\theta_s - \theta_e)$$

:

$$P_e = C_p \cdot (\theta_{moy} - \theta_a)$$

:

$$\theta_{moy} = \frac{3\theta_s + \theta_e}{4} + \Delta\theta$$

:() Pa, Pu, Pe

$$E \cdot \rho \cdot \alpha \cdot \tau \cdot C = q \cdot C \cdot (\theta_s - \theta_e) + C_p \left[\frac{3\theta_s + \theta_e}{4} + \Delta\theta - \theta_a \right]$$

$\Delta\theta$

:

()

$$C_P = h_r + h_C + h_{ar}$$

:

: h_{ar}

()

$$h_{ar} = \frac{S_r}{s} \frac{\lambda_{ar}}{e} \frac{(\theta_{moy} - \theta_{ar})}{(\theta_{moy} - \theta_a)}$$

:

: h_{r1} h_{c1} : h_{r2} h_{c2}

:

$$h_{r1} = \varepsilon_{ac} \cdot \sigma \frac{(T_{moy}^4 - T_{Cmoy}^4)}{T_{moy} - T_{Cmoy}}$$

$$h_{c1} = 3,30 \text{ W/m}^2.K$$

$$h_{r2} = \frac{\varepsilon_C \cdot \sigma (T_{cmoy}^4 - T_a^4)}{T_{Cmoy} - T_a}$$

$$h_{c2} = 7,5 + 4V$$

$$0 < V < 4 \text{ m/s}$$

$$h_{c2} = 7,3 V^{0,30}$$

$$4 < V < 40 \text{ m/s}$$

$$\varepsilon_{ac} = \frac{I}{\frac{I}{\varepsilon_a} + \frac{I}{\varepsilon_C} - I}$$

:

$$h_r + h_C = \frac{I}{\frac{I}{h_{c1} + h_{r1}} + \frac{I}{h_{r2} + h_{c2}}}$$

:

()
$$\eta = \frac{P_u}{C \cdot E}$$

()
$$\eta = \rho \cdot \tau \cdot \alpha - \frac{C_p(\theta_{moy} - \theta_a)}{C \cdot E}$$

:

()
$$\eta_i = \frac{P_u}{P_a}$$

: [Pasquetti, R., 1987]

()
$$C_{e_{max}} = \frac{\sin \theta}{\pi \cdot \sin \gamma_t}$$

:

$$/\pi = \theta$$

$$C_{e_{max}} = \frac{1}{\pi \cdot \sin \gamma_t}$$

: [Welford, W.T., Winston R., 1978]

$$\theta = 2 \text{ Arc tg}[D/4f]$$

$$f = \frac{D}{4 \text{tg}(\frac{\theta}{2})}$$

: f

:

$$y^2 = 4f \cdot x$$

:

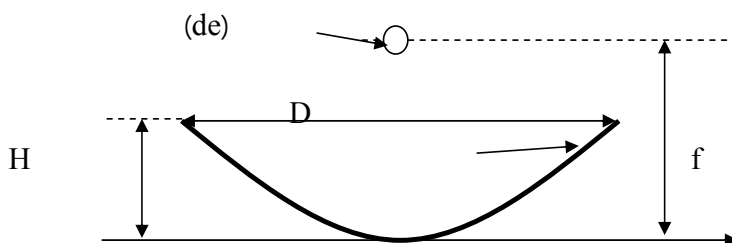
$$(D/2)^2 = 4f \cdot H$$

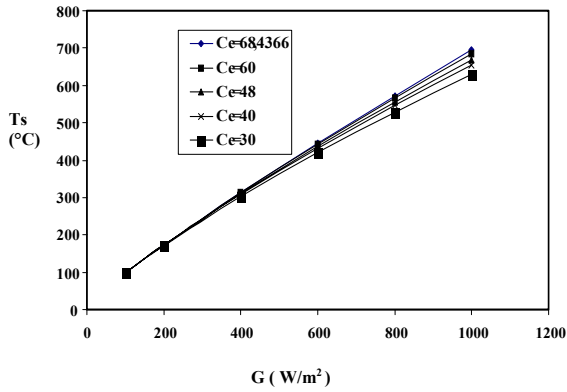
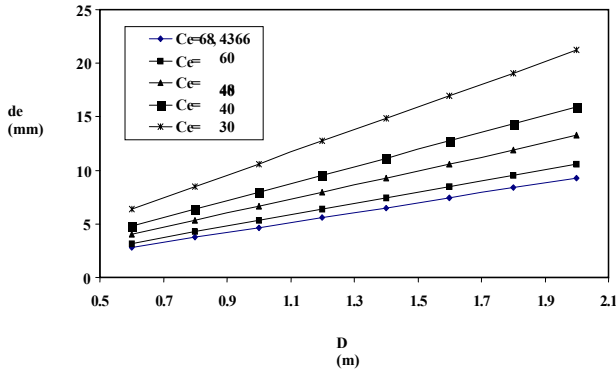
:H

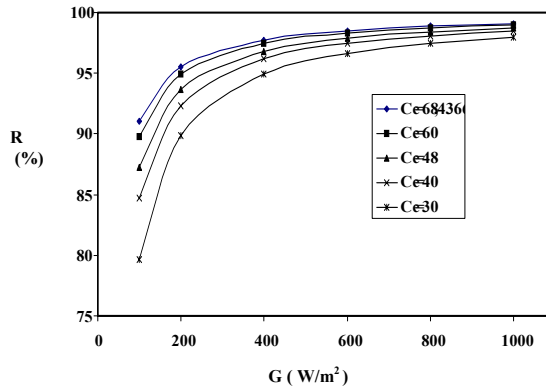
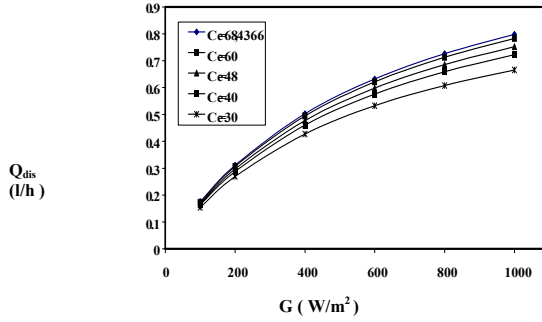
$$H = D^2 / (16 \cdot f)$$

[Bouges, B., 1992] "Euftrat"

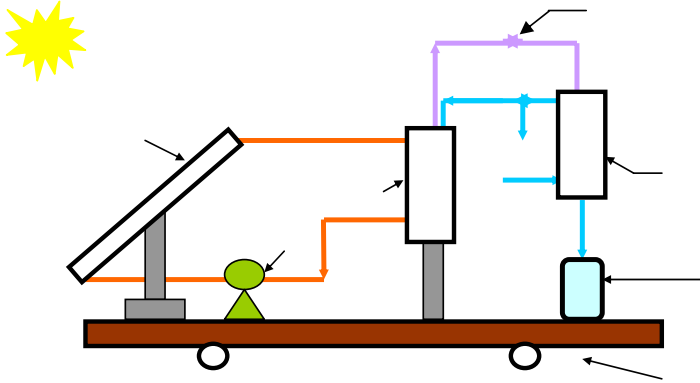
(W/m ²) -	
(l/h) , - ,	
, -	
(°C) -	







(f=H)



:

()

($C_e = 1$)

:

:

$$n = S/s$$

.S

n.s

:

$$R = l/n$$

(v)

S:

$$r = v.s/S$$

()

:

$$(G = 700 \text{ W/m}^2)$$

()	()		
,	,		
s = ,	,	,	
S = ,	,	-	*

*

, %

(J/kg°C)			: C
(W/m ² °C)			: Cp
(m)			: D
(W/m ²)			: E
(m)			: e
(W/m ²)			: G
(m)			: f
(m)			: H
(W/m ² °C)			: h
(ans)			: n
(m)			: L
(kg/s)			: q
(W/m ²)			: P
(%)			: R
(m ²)			: Sr
(\$)			: S
(m ²)			: s
(an/\$)			: s
(K)			: T
(ans)			: v
(C°)			: θ
(W/m ² °C)			: λ
(°)			: γ
			: α
			: τ
(W/m ² K ⁴)	5.67 10 ⁻⁸	STEFAN	: σ
			: ε

: a

:ac

ar :

: c

: cmoy

: e

: s

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