

Consider a stationary control volume through which a fluid is moving. The general energy balance equation:

$$\begin{aligned}
 & \left. \begin{array}{l} \textcircled{1} \\ \text{Rate of} \\ \text{Accumulation.} \\ \underline{KE + Int. E} \end{array} \right\} = \left. \begin{array}{l} \textcircled{2} \\ \text{Rate of Energy} \\ \text{Addition by} \\ \text{Convection.} \\ \underline{KE + Int. E} \end{array} \right\} + \left. \begin{array}{l} \textcircled{3} \\ \text{Rate of Energy} \\ \text{Addition by} \\ \text{Molecular Transp.} \\ \underline{Conduction} \end{array} \right\} \\
 & \qquad \qquad \qquad \left. \begin{array}{l} \textcircled{4} \\ \text{Rate of Work} \\ \text{done on system} \\ \text{by molecular} \\ \text{Mechanisms} \\ \text{(i.e. stress + pressure)} \end{array} \right\} + \left. \begin{array}{l} \textcircled{5} \\ \text{Rate of work} \\ \text{done on system} \\ \text{by external} \\ \text{forces (gravity)} \end{array} \right\}
 \end{aligned}$$

before we proceed we introduce the Combined

Energy Flux Vector, \vec{e} :

$$\vec{e} \left(\frac{J}{m^2 s} \right) = \underbrace{\frac{1}{2} \rho v^2 \vec{v}}_{KE} + \underbrace{\rho \hat{U} \vec{v}}_{Int. E.} + \underbrace{P \vec{v}}_{\text{work due to pressure}} + \underbrace{\underline{\tau} \cdot \vec{v}}_{\text{work due to stress}} + \underbrace{\vec{q}}_{\text{conduction}}$$

note: $v^2 = \vec{v} \cdot \vec{v} = v_x^2 + v_y^2 + v_z^2$

add all terms :

(2)

$$\Delta x \Delta y \Delta z \frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 + \rho \hat{U} \right) = \left(e_x|_x - e_x|_{x+\Delta x} \right) \Delta y \Delta z + \left(e_y|_y - e_y|_{y+\Delta y} \right) \Delta x \Delta z + \left(e_z|_z - e_z|_{z+\Delta z} \right) \Delta x \Delta y + \rho \Delta x \Delta y \Delta z \left(\vec{V} \cdot \vec{g} \right)$$

\div by $\Delta x \Delta y \Delta z$ and $\Delta x \Delta y \Delta z \rightarrow 0$

$$\frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 + \rho \hat{U} \right) = - \vec{\nabla} \cdot \vec{e} + \rho \left(\vec{g} \cdot \vec{V} \right) \quad \left(\frac{\text{J}}{\text{m}^3 \text{ s}} \right)$$

recall definition of \vec{e} (energy flux vector)

⋮

$\frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 + \rho \hat{U} \right) =$	$-\vec{\nabla} \cdot \left(\frac{1}{2} \rho v^2 + \rho \hat{U} \right) \vec{V}$	Convection
	$-\vec{\nabla} \cdot \vec{q}$	Conduction
	$-\vec{\nabla} \cdot p \vec{V}$	Work due to Pressure
	$-\vec{\nabla} \cdot \left[\underline{\underline{e}} \cdot \vec{V} \right]$	Work due to Friction
	$+\rho \left(\vec{V} \cdot \vec{g} \right)$	Work by external forces

..... Eq. (1)

Recall the equation of motion:

(3)

$$\frac{\partial}{\partial t} \rho \vec{v} = - \vec{\nabla} \cdot \rho \vec{v} \vec{v} - \vec{\nabla} p - \vec{\nabla} \cdot \underline{\underline{\tau}} + \rho \vec{g} \quad \left(\frac{N}{m^3} \right)$$

take dot product with \vec{v}

o
o
o

$$\frac{\partial}{\partial t} \left(\frac{1}{2} \rho v^2 \right) = - \vec{\nabla} \cdot \frac{1}{2} \rho v^2 \vec{v} - \vec{\nabla} \cdot p \vec{v} - p (-\vec{\nabla} \cdot \vec{v}) - \vec{\nabla} \cdot (\underline{\underline{\tau}} \cdot \vec{v}) - (-\underline{\underline{\tau}} : \vec{\nabla} \vec{v}) + \rho (\vec{v} \cdot \vec{g}) \quad \text{Eq. (2)}$$

$\left(\frac{J}{m^3 s} \right)$

Eq. (1) Combines both mechanical energy and internal energy

Eq. (2) Mechanical Energy equation

Eq. (1) - Eq. (2) :

$$\frac{\partial}{\partial t} (\rho \hat{U}) = - \vec{\nabla} \cdot \rho \hat{U} \vec{v} - \vec{\nabla} \cdot \vec{q} - p (\vec{\nabla} \cdot \vec{v}) - \underline{\underline{\tau}} : \underline{\underline{\nabla}} \vec{v} \quad \text{Eq. (3)}$$

Equation (3) Internal Energy equation and it is useful to obtain energy equation in terms of temperature

Rearranging by utilizing substantial derivative (4)

∴

$$\rho \frac{D\hat{U}}{Dt} = -\vec{\nabla} \cdot \vec{q} - p(\vec{\nabla} \cdot \vec{v}) - \underline{\underline{\rho : \underline{\underline{\nabla v}}}}$$

Enthalpy $\hat{H} = \hat{U} + p\hat{V}$

↑
specific volume ($\frac{1}{\rho}$)

∴

$$\rho \frac{D\hat{H}}{Dt} = -(\vec{\nabla} \cdot \vec{q}) - (\underline{\underline{\rho : \underline{\underline{\nabla v}}}}) + \frac{Dp}{Dt}$$

recall from thermodynamics :

$$d\hat{H} = c_p dT + \left[\hat{V} - T \left(\frac{\partial \hat{V}}{\partial T} \right)_p \right] dp$$

$$= c_p dT + \left[\frac{1}{\rho} + \left(\frac{\partial \ln p}{\partial \ln T} \right)_p \right] dp$$

→ = 1 for ideal gas.

$$\Rightarrow \rho c_p \frac{DT}{Dt} = -\vec{\nabla} \cdot \vec{q} - (\underline{\underline{\rho : \underline{\underline{\nabla v}}}}) - \left(\frac{\partial \ln p}{\partial \ln T} \right)_p \frac{Dp}{Dt}$$

The Energy Equation.

Special Forms of Energy Equation:

(5)

① Constant density fluids

$$\rho C_p \frac{DT}{Dt} = -\nabla \cdot \vec{q} - \underline{\underline{\dot{\Sigma}}} : \underline{\underline{\nabla V}}$$

② Newtonian Fluids:

$$\underline{\underline{\dot{\Sigma}}} : \underline{\underline{\nabla V}} = \mu \underline{\underline{\Phi}}_v + \kappa \psi \quad \psi = (\nabla \cdot v)^2$$

see Appendix B.7

$$\rho C_p \frac{DT}{Dt} = -\nabla \cdot \vec{q} - (\mu \underline{\underline{\Phi}}_v + \kappa \psi) - \left(\frac{\partial \ln \rho}{\partial \ln T} \right)_p \frac{DP}{Dt}$$

③ Materials following Fourier's law of conduction

$$\vec{q} = -k \nabla T$$

if k is const

$$\rho C_p \frac{DT}{Dt} = k \nabla^2 T - (\mu \underline{\underline{\Phi}}_v + \kappa \psi) - \left(\frac{\partial \ln \rho}{\partial \ln T} \right)_p \frac{DP}{Dt}$$

④ Const. ρ , Newtonian, Fourier's law \leftarrow Incompressible flow

$$\rho C_p \frac{DT}{Dt} = k \nabla^2 T - \mu \underline{\underline{\Phi}}_v$$