Handout_15 **Annular Flow** Dr. Usamah Al-Mubaiyedh

Example 6.5—Flow Through an Annular Die

Following the discussion of polymer processing in the previous section, now consider flow through a die that could be located at the exit of the screw extruder of Example 6.4. Consider a die that forms a tube of polymer (other shapes being sheets and filaments). In the die of length (shown in Fig. E6.5, a pressure difference $p_2 - p_3$ causes a liquid of viscosity μ to flow steadily from left to right in the annular area between two fixed concentric cylinders. Note that p_2 is chosen for the inlet pressure in order to correspond to the extruder exit pressure from Example 6.4. The inner cylinder is solid, whereas the outer one is hollow; their radii are r_1 and r_2 , respectively. The problem, which could occur in the extrusion of plastic tubes, is to find the velocity profile in the annular space and the total volumetric flow rate Q. Note that cylindrical coordinates are now involved.

Assumptions and continuity equation. The following assumptions are realistic:

- 1. There is only one nonzero velocity component, namely that in the direction of flow, v_z . Thus, $v_r = v_\theta = 0$.
- 2. Gravity acts vertically downwards, so that $g_z = 0$.
- 3. The axial velocity is independent of the angular location; that is, $\partial v_z/\partial\theta = 0$.

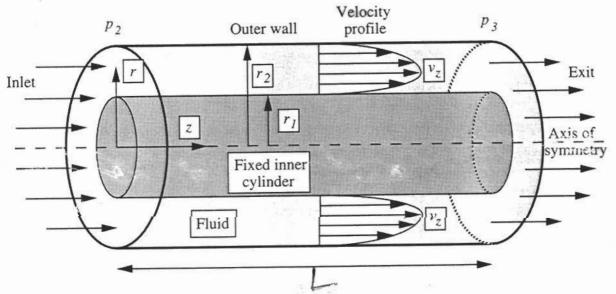


Fig. E6.5 Geometry for flow through an annular die.

Soluhon:

Continuity equation: $\frac{\partial f}{\partial t} + \frac{1}{r} \frac{\partial (\rho r b_r)}{\partial r} + \frac{1}{r} \frac{\partial (\rho b_\theta)}{\partial \theta} + \frac{\partial (\rho v_z)}{\partial z} = 0,$

=) $\frac{\partial V_2}{\partial z} = 0$, $V_2 \neq f(z)$ also for axisymmetric flow $V_2 \neq f(z) = V_2 = f(r)$ only.

Navier-Stokes Equalbas:

$$V_r = V_0 = 0$$
) $\frac{\partial}{\partial a}(any + hing) = 0$ [axisymmetric] problem] SS_r and $V_2 = f(r)$ only.

$$\begin{split} \rho \Big(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \Big) \\ &= -\frac{\partial p}{\partial r} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (rv_r)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right] + \rho g_r, \end{split}$$

$$\begin{split} \rho \Big(\frac{\partial v_{\theta}}{\partial t} + v_{r} \frac{\partial v_{\theta}}{\partial r} + \frac{v_{\theta}}{r} \frac{\partial v_{\theta}}{\partial \theta} + \frac{v_{r} v_{\theta}}{r} + v_{z} \frac{\partial v_{\theta}}{\partial z} \Big) \\ &= -\frac{1}{r} \frac{\partial p}{\partial \theta} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (r v_{\theta})}{\partial r} \right) + \frac{1}{r^{2}} \frac{\partial^{2} v_{\theta}}{\partial \theta^{2}} + \frac{2}{r^{2}} \frac{\partial v_{r}}{\partial \theta} + \frac{\partial^{2} v_{\theta}}{\partial z^{2}} \right] + \rho g_{\theta}, \end{split}$$

$$\begin{split} \rho \Big(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \Big) \\ &= -\frac{\partial p}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z. \end{split}$$

pressure variation in 2-direction is linear

=>
$$\frac{1}{r} \frac{d}{dr} \left(r \frac{dV_2}{dr} \right) = \frac{\Delta P}{\mu L}$$

integrate twice:

boundary conditions:

$$r = r_1$$
 $V_2 = 0$ (no-slip BC)
 $r = r_2$ $V_2 = 0$ (no-slip BC)

$$\Rightarrow 0 = \frac{\Delta P}{4\mu L} r_1^2 + c_1 \ln(r_1) + c_2 - - - 0$$

$$0 = \frac{\Delta P}{4\mu L} r_2^2 + c_1 \ln(r_2) + c_2 - - \cdot (2)$$

1 - 0 =>
$$\frac{\Delta P}{4ML} \left(r_1^2 - r_2^2 \right) + c_1 lm \left(\frac{r_1}{r_2} \right) = 0$$

$$= > C_1 = \frac{\Delta P}{4uL} \left(r_2^2 - r_1^2 \right) \\ Ln \left(\frac{r_1}{r_2} \right)$$

substitute in ②:

$$c_2 = -\frac{\Delta P}{4ML} r_2^2 - \frac{\Delta P}{4ML} \left(r_2^2 - r_1^2\right) \ln \left(r_2\right)$$

substitute as cz in velocity profile

$$= V_2 = \frac{\Delta P}{4ML} \left[\left(r^2 - r_2^2 \right) + \frac{r_2^2 - r_1^2}{m \left(\frac{r_1}{r_2} \right)} m \left(\frac{r}{r_2} \right) \right]$$

Volumetric flow rache

$$Q = \int_A V_2 dA$$

$$Q = \int_{0}^{2\pi} \int_{1}^{r_{2}} V_{2} r dr dQ$$

$$Q = \frac{\pi \left(r_{2}^{2} - r_{1}^{2}\right)}{8 M} \frac{\Delta P}{L} \left[\frac{r_{2}^{2} - r_{1}^{2}}{m \left(\frac{r_{2}}{r_{1}}\right)} - \left(r_{2}^{2} + r_{1}^{2}\right)\right]$$

Stress Tensor:

recall
$$V_r = V_R = 0$$
 $\frac{\partial}{\partial \alpha}() = 0$ $V_2 = F(r)$ only

$$\tau_{r\theta} = \tau_{\theta r} = \mu \left(r \frac{\partial}{\partial r} \left(\frac{v_{\theta}}{r} \right) + \frac{1}{r} \frac{\partial v_{r}}{\partial \theta} \right),$$

$$\tau_{\theta z} = \tau_{z\theta} = \mu \left(\frac{\partial v_{\theta}}{\partial z} + \frac{1}{r} \frac{\partial v_{z}}{\partial \theta} \right),$$

$$\tau_{zr} = \tau_{rz} = \mu \left(\frac{\partial v_{z}}{\partial r} + \frac{\partial v_{z}}{\partial z} \right).$$

$$\sigma_{rr} = -p + 2\mu \frac{\partial v_{r}}{\partial r} - \frac{2}{3}\mu \nabla \cdot \nabla,$$

$$\sigma_{\theta\theta} = -p + 2\mu \left(\frac{1}{r} \frac{\partial v_{\theta}}{\partial \theta} + \frac{v_{r}}{r} \right) - \frac{2}{3}\mu \nabla \cdot \nabla,$$

$$\sigma_{zz} = -p + 2\mu \frac{\partial v_{z}}{\partial z} - \frac{2}{3}\mu \nabla \cdot \nabla.$$

$$\mathcal{Z}_{rz} = \mathcal{Z}_{zr} = \mu \frac{dV_z}{dr} \\
= \frac{\Delta P}{4L} \left[2r + \frac{r_z^2 - r_i^2}{m(\frac{r_i}{r_z})} \frac{1}{r} \right]$$