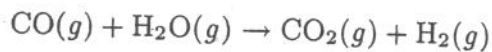


Example 13.5 The water-gas-shift reaction



is carried out under the different sets of conditions described below. Calculate the fraction of steam reacted in each case. Assume the mixture behaves as an ideal gas.

- The reactants consist of 1 mol of  $\text{H}_2\text{O}$  vapor and 1 mol of  $\text{CO}$ . The temperature is 1100 K and the pressure is 1 bar.
- Same as (a) except that the pressure is 10 bar.
- Same as (a) except that 2 mol of  $\text{N}_2$  is included in the reactants.
- The reactants are 2 mol of  $\text{H}_2\text{O}$  and 1 mol of  $\text{CO}$ . Other conditions are the same as in (a).
- The reactants are 1 mol of  $\text{H}_2\text{O}$  and 2 mol of  $\text{CO}$ . Other conditions are the same as in (a).
- The initial mixture consists of 1 mol of  $\text{H}_2\text{O}$ , 1 mol of  $\text{CO}$ , and 1 mol of  $\text{CO}_2$ . Other conditions are the same as in (a).
- Same as (a) except that the temperature is 1650 K.

(a) First  $K$  need to be calculated at 1100K

$$\Delta H^\circ = -393509 + 0 - (-110525) - (-241818) = -41161$$

$$\Delta G^\circ = -394359 + 0 - (-137169) - (-228572) = -28618 \frac{\text{J}}{\text{mol}}$$

$$K_0 = e^{\left(\frac{-\Delta G^\circ}{RT_0}\right)} = e^{\left(\frac{28618}{(8.314)(298.15)}\right)} = 103260.84$$

assume  $\Delta H^\circ$  constant.

$$\ln\left(\frac{K}{103260.84}\right) = \frac{41161}{8.314} \left(\frac{1}{1100} - \frac{1}{298.15}\right)$$

$$\Rightarrow K = 0.6$$

# equilibrium relation

$$K \left( \frac{P}{P^0} \right)^{-\nu} = \prod_i (y_i)^{\nu_i} \quad (\text{ideal gas. assumption})$$

$$P = 1 \text{ bar}, \quad P^0 = 1 \text{ bar} \quad \& \quad \nu = 1 + 1 - 1 - 1 = 0,$$

$$\Rightarrow 0.6 = \frac{y_{\text{H}_2} y_{\text{CO}_2}}{y_{\text{CO}} y_{\text{H}_2\text{O}}} \quad (1)$$

$$y_i = \frac{n_i}{n} = \frac{n_{i0} + \nu_i \varepsilon}{n_0 + \gamma \varepsilon}$$

$$\text{at equilibrium} \quad y_i = \frac{n_{i0} + \nu_i \varepsilon_e}{n_0 + \gamma \varepsilon_e}$$

$$y_{\text{H}_2} = \frac{\varepsilon_e}{2} \quad y_{\text{CO}_2} = \frac{\varepsilon_e}{2}$$

$$y_{\text{CO}} = \frac{1 - \varepsilon_e}{2} \quad y_{\text{H}_2\text{O}} = \frac{1 - \varepsilon_e}{2}$$

substitute in equation (1) above

$$0.6 = \frac{\left( \frac{\varepsilon_e}{2} \right) \left( \frac{\varepsilon_e}{2} \right)}{\left( \frac{1 - \varepsilon_e}{2} \right) \left( \frac{1 - \varepsilon_e}{2} \right)} = \frac{\varepsilon_e^2}{(1 - \varepsilon_e)^2}$$

$$0.6 (\varepsilon_e^2 - 2\varepsilon_e + 1) = \varepsilon_e^2$$

$$0.4 \cdot \xi_e^2 + 1.2 \xi_e - 0.6 = 0$$

$$\xi_e = \frac{-1.2 + \sqrt{1.2^2 + 4(0.4)(0.6)}}{0.8} = 0.44$$

$$X_{\text{steam}} = \text{fraction reacted} = \frac{(n_{\text{H}_2\text{O}})_0 - \text{H}_2\text{O}}{(n_{\text{H}_2\text{O}})_0}$$

$$X_{\text{steam}} = \frac{1 - ((n_{\text{H}_2\text{O}})_0 - \xi_e)}{1} = 0.44$$

44% reacts at equilibrium.

(b)  $p = 10$  bar

$$K \left( \frac{p}{p^0} \right)^{-\nu} = \prod_i (y_i)^{\nu_i}$$

$$\text{since } \nu = 0 \Rightarrow K = \prod_i (y_i)^{\nu_i}$$

solution is exactly similar to (a)

(c) 2 moles  $\text{N}_2$  added (inert gas)

$$K \left( \frac{p}{p^0} \right)^{-\nu} = \prod_i (y_i)^{\nu_i}$$

$$0.6 = \frac{y_{\text{H}_2} y_{\text{CO}_2}}{y_{\text{CO}} y_{\text{H}_2\text{O}}}$$

$$y_{H_2} = \frac{\epsilon_e}{4}$$

$$y_{CO_2} = \frac{\epsilon_e}{4}$$

(6)

$$y_{CO} = \frac{1 - \epsilon_e}{4}$$

$$y_{H_2O} = \frac{1 - \epsilon_e}{4}$$

$$\Rightarrow 0.6 = \frac{\epsilon_e^2}{(1 - \epsilon_e)^2}$$

$\Rightarrow$  result similar to (a)

(d) 2 mole  $H_2O$  & 1 mol  $CO$  initially

$$0.6 = \frac{y_{H_2} y_{CO_2}}{y_{CO} y_{H_2O}}$$

$$y_{CO} = \frac{1 - \epsilon_e}{3}$$

$$y_{H_2O} = \frac{2 - \epsilon_e}{3}$$

$$y_{CO_2} = \frac{\epsilon_e}{3}$$

$$y_{H_2} = \frac{\epsilon_e}{3}$$

$$\Rightarrow 0.6 = \frac{\epsilon_e^2}{(1 - \epsilon_e)(2 - \epsilon_e)}$$

$$\Rightarrow 0.4 \epsilon_e^2 + 1.8 \epsilon_e - 1.2 = 0 \quad \Rightarrow \epsilon_e = 0.59$$

$$X_{\text{steam}} = \frac{n_{O_{H_2O}} - (n_{O_{H_2O}} - \epsilon_e)}{n_{O_{H_2O}}} = 0.295$$

(e) 1 mole  $H_2O$  2 kmol  $CO_2$  initially (4)

$$0.6 = \frac{\frac{\xi_e}{3}}{\frac{(2-\xi_e)}{3} + \frac{(1-\xi_e)}{3}}$$

$$\Rightarrow \xi_e = 0.59$$

$$X_{steam} = \frac{n_{O_{H_2O}} - (n_{O_{H_2O}} - \xi_e)}{n_{O_{H_2O}}} = 0.59$$

$$(f) \quad 0.6 = \frac{y_{H_2} y_{CO_2}}{y_{CO} y_{H_2O}} = \frac{\xi_e (1+\xi_e)}{(1-\xi_e)^2}$$

$$0.4 \xi_e^2 + 2.2 \xi_e - 0.6 = 0$$

$$\Rightarrow \xi_e = 0.26$$

$$X_{steam} = \frac{n_{O_{H_2O}} - (n_{O_{H_2O}} - \xi_e)}{n_{O_{H_2O}}} = 0.26$$

$$(g) \quad \ln\left(\frac{K}{103260.84}\right) = \frac{41161}{8.314} \left(\frac{1}{1650} - \frac{1}{298.15}\right)$$

$$\Rightarrow K = 0.13$$

$$\Rightarrow 0.13 = \frac{\xi_e^2}{(1-\xi_e)^2} \Rightarrow \xi_e = 0.27 \Rightarrow X = 0.27$$