

$$\text{Basis: } n_0 = \frac{200 \text{ kPa}}{1 \text{ kPa}} \left| \frac{1000 \text{ Pa}}{1 \text{ kPa}} \right| \left| \frac{10 \text{ L}}{1 \text{ L}} \right| \left| \frac{10^{-3} \text{ m}^3}{1 \text{ L}} \right| \left| \frac{1 \text{ mol K}}{8.314 \text{ m}^3 \text{ Pa}} \right| \left| \frac{298 \text{ K}}{298 \text{ K}} \right| \\ = 0.8072 \text{ mol feed gas mixture}$$

$$0.8072 \text{ mol feed gas mixture} \Rightarrow (0.85)(0.8072) = 0.6861 \text{ mol CH}_4, \\ \Rightarrow (0.15)(0.8072) = 0.1211 \text{ mol O}_2$$

$$\text{CH}_4 \text{ consumed: } \frac{1 \text{ mol CH}_4}{1 \text{ mol O}_2 \text{ fed}} = 0.1211 \text{ mol CH}_4$$

$$\Rightarrow n_5 = (0.6861 - 0.1211) \text{ mol CH}_4 = 0.5650 \text{ mol CH}_4$$

$$\text{HCHO produced: } n_3 = \frac{1 \text{ mol HCHO}}{1 \text{ mol CH}_4 \text{ consumed}} = 0.1211 \text{ mol HCHO}$$

$$\text{H}_2\text{O produced: } n_4 = \frac{1 \text{ mol H}_2\text{O}}{1 \text{ mol CH}_4 \text{ consumed}} = 0.1211 \text{ mol H}_2\text{O}$$

$$\text{Extent of reaction: } \xi = \frac{|(n_{O_2})_{\text{out}} - (n_{O_2})_{\text{in}}|}{|v_{O_2}|} = \frac{|0 - 0.1211|}{|1|} = 0.1211 \text{ mol}$$

References: $\text{CH}_4(\text{g}), \text{O}_2(\text{g}), \text{HCHO}(\text{g}), \text{H}_2\text{O}(\text{g})$, at 25°C

| Substance | n_{in} mol | \dot{U}_{in} kJ/mol | n_{out} mol | \dot{U}_{out} kJ/mol |
|----------------------|------------------------|---------------------------------|-------------------------|----------------------------------|
| CH_4 | 0.6861 | 0 | 0.5650 | \dot{U}_1 |
| O_2 | 0.1211 | 0 | — | — |
| HCHO | — | — | 0.1211 | \dot{U}_2 |
| H_2O | — | — | 0.1211 | \dot{U}_3 |

$$\dot{U}_i = \int_{25}^{T_f} (C_p)_i dT = \int_{25}^{T_f} (C_p - R)_i dT \quad i = 1, 2, 3$$

Using $(C_p)_i$ from Table B.2 and $R = 8.314 \times 10^{-3} \text{ kJ/mol}\cdot\text{K}$:

$$\dot{U}_1 = (0.02599 T + 2.7345 \times 10^{-3} T^2 + 0.1220 \times 10^{-8} T^3 - 2.75 \times 10^{-12} T^4 - 0.6670) \text{ kJ/mol}$$

$$\dot{U}_2 = (0.02597 T + 2.1340 \times 10^{-3} T^2 - 2.1735 \times 10^{-12} T^4 - 0.6623) \text{ kJ/mol}$$

$$\dot{U}_3 = (0.02515 T + 0.3440 \times 10^{-3} T^2 + 0.2535 \times 10^{-8} T^3 - 0.8983 \times 10^{-12} T^4 - 0.6309) \text{ kJ/mol}$$

$$Q = \frac{100 \text{ J}}{\text{s}} \left| \frac{85 \text{ s}}{1000 \text{ J}} \right| = 8.5 \text{ kJ}$$

Table B.1

$$\Delta \hat{H}_r^\ominus = (\Delta \hat{H}_r^\ominus)_{\text{HCHO}} + (\Delta \hat{H}_r^\ominus)_{\text{H}_2\text{O}} - (\Delta \hat{H}_r^\ominus)_{\text{CH}_4} = ((-115.90) + (-241.83) - (-74.85)) \text{ kJ/mol}$$

$$= -282.88 \text{ kJ/mol}$$

$$\Delta \dot{U}_r^\ominus = \Delta \hat{H}_r^\ominus - RT \left(\sum_{\text{gaseous products}} v_i - \sum_{\text{gaseous reactants}} v_i \right)$$

$$= -282.88 \text{ kJ/mol} - \frac{8.314 \text{ J}}{\text{mol K}} \left| \frac{298 \text{ K}}{1000 \text{ J}} \right| (1 + 1 - 1 - 1) = -282.88 \text{ kJ/mol}$$

Energy Balance :

$$\begin{aligned} Q &= \xi \Delta \hat{U}_r^{\circ} + \sum (n_i)_{\text{out}} (\hat{U}_i)_{\text{out}} - \sum (n_i)_{\text{in}} (\hat{U}_i)_{\text{in}} \\ &= (0.1211)(-282.88 \text{ kJ/mol}) + 0.5650 \hat{U}_1 + 0.1211 \hat{U}_2 + 0.1211 \hat{U}_3 \end{aligned}$$

↓ Substitute for \hat{U}_1 through \hat{U}_3 and Q

$$0 = 0.02088 T + 1.845 \times 10^{-5} T^2 + 0.09963 \times 10^{-8} T^3 - 1.926 \times 10^{-12} T^4 - 43.29 \text{ kJ/mol}$$

Solve for T using E - Z Solve $\Rightarrow T = 1091^\circ \text{C} = 1364 \text{ K}$

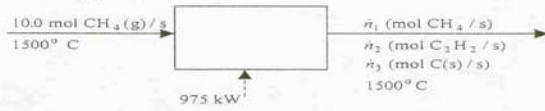
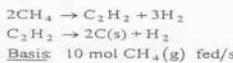
$$\Rightarrow P = nRT/V = \frac{0.8072 \text{ mol}}{\text{mol} \cdot \text{K}} \left| \frac{8.314 \text{ m}^3 \cdot \text{Pa}}{10 \text{ L}} \right| \left| \frac{1364 \text{ K}}{10^{-3} \text{ m}^3} \right| = 915 \times 10^3 \text{ Pa} = \underline{\underline{915 \text{ kPa}}}$$

Add heat to raise the reactants to a temperature at which the reaction rate is significant.

b. Side reaction: $\text{CH}_4 + 2\text{O}_2 \rightarrow \text{CO}_2 + 2\text{H}_2\text{O}$. T would have been higher (more negative heat of

c. reaction for combustion of methane), volume and total moles would be the same, therefore
 $P = nRT/V$ would be greater.

9.36



a. $60\% \text{ conversion} \Rightarrow \dot{n}_1 = 10(1 - 0.600) = 4.00 \text{ mol CH}_4/\text{s}$

C balance: $10(1) = 4(1) + 2\dot{n}_2 + \dot{n}_4 \Rightarrow 2\dot{n}_2 + \dot{n}_4 = 6 \quad (1)$

H balance: $10(4) = 4(4) + 2\dot{n}_3 + 2\dot{n}_4 \Rightarrow 2\dot{n}_3 + 2\dot{n}_4 = 24 \quad (2)$

References for enthalpy calculations: C(s), H₂(g) at 25°C

$$H_i = (\Delta\hat{H}_f^o)_i + C_{pi}(1500 - 25), i = \text{CH}_4, \text{C}_2\text{H}_2, \text{C}, \text{H}_2$$

| Substance | \dot{n}_{in} (mol/s) | \dot{H}_{in} (kJ/mol) | \dot{n}_{out} (mol/s) | \dot{H}_{out} (kJ/mol) |
|-----------------------------------|---------------------------|----------------------------|----------------------------|-----------------------------|
| CH ₄ (g) | 10 | 41.68 | 4 | 41.68 |
| C ₂ H ₂ (g) | — | — | \dot{n}_2 | 303.45 |
| H ₂ (g) | — | — | \dot{n}_3 | 45.72 |
| C(s) | — | — | \dot{n}_4 | 32.45 |

Energy Balance: $Q = \Delta H \Rightarrow 975 \text{ kJ/s} = \sum_{out} \dot{n}_i \dot{H}_i - \sum_{in} \dot{n}_i \dot{H}_i \quad (3)$

Solve (1) - (3) simultaneously $\Rightarrow \begin{cases} \dot{n}_2 = 2.50 \text{ mol C}_2\text{H}_2/\text{s} \\ \dot{n}_3 = 9.50 \text{ mol H}_2/\text{s} \\ \dot{n}_4 = 1.00 \text{ mol C/s} \end{cases}$

Yield of acetylene = $\frac{2.50 \text{ mol C}_2\text{H}_2/\text{s}}{6.00 \text{ mol CH}_4 \text{ consumed/s}} = 0.417 \text{ mol C}_2\text{H}_2/\text{mol CH}_4 \text{ consumed}$

b. If no side reaction,

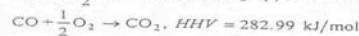
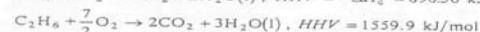
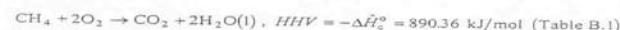
$\dot{n}_1 = 10.0(1 - 0.600) = 4.00 \text{ mol CH}_4/\text{s}$

$\dot{n}_3 = 0 \Rightarrow \dot{n}_2 = 3.00 \text{ mol C}_2\text{H}_2/\text{s}, \dot{n}_4 = 9.00 \text{ mol H}_2/\text{s}$

Yield of acetylene = $\frac{3.00 \text{ mol C}_2\text{H}_2/\text{s}}{6.00 \text{ mol CH}_4 \text{ consumed/s}} = 0.500 \text{ mol C}_2\text{H}_2/\text{mol CH}_4 \text{ consumed}$

Reactor Efficiency = $\frac{0.417}{0.500} = 0.834$

9.50



$$\begin{array}{c|c|c|c|c} \text{Initial moles charged:} & 2.000 \text{ L} & 273.2 \text{ K} & 2323 \text{ mm Hg} & 1 \text{ mol} \\ \hline (\text{Assume ideal gas}) & & (25 + 273.2) \text{ K} & 760 \text{ mm Hg} & 22.4 \text{ L(STP)} \end{array} = 0.25 \text{ mol}$$

Average mol. wt._{av} (4.929 g)/(0.25 mol) = 19.72 g/mol

Let $x_1 = \text{mol CH}_4/\text{mol gas}, x_2 = \text{mol C}_2\text{H}_6/\text{mol gas} (\Rightarrow (1-x_1-x_2)\text{mol CO(mol gas)})$

$$\overline{MW} = 19.72 \Rightarrow x_1(16.04 \text{ g/mol CH}_4) + x_2(30.07) + (1-x_1-x_2)(28.01) = 19.72 \quad (1)$$

$$\text{HHV} = 963.7 \text{ kJ/mol} \Rightarrow x_1(890.36) + x_2(1559.9) + (1-x_1-x_2)(282.99) = 963.7 \quad (2)$$

Solving (1) & (2) simultaneously yields

$$x_1 = 0.725 \text{ mol CH}_4/\text{mol}, x_2 = 0.188 \text{ mol C}_2\text{H}_6/\text{mol}, 1-x_1-x_2 = 0.087 \text{ mol CO/mol}$$