

Example 6.5—Flow Through an Annular Die

Following the discussion of polymer processing in the previous section, now consider flow through a die that could be located at the exit of the screw extruder of Example 6.4. Consider a die that forms a *tube* of polymer (other shapes being sheets and filaments). In the die of length L shown in Fig. E6.5, a pressure difference $p_2 - p_3$ causes a liquid of viscosity μ to flow steadily from left to right in the annular area between two fixed concentric cylinders. Note that p_2 is chosen for the inlet pressure in order to correspond to the extruder exit pressure from Example 6.4. The inner cylinder is solid, whereas the outer one is hollow; their radii are r_1 and r_2 , respectively. The problem, which could occur in the extrusion of plastic tubes, is to find the velocity profile in the annular space and the total volumetric flow rate Q . Note that *cylindrical* coordinates are now involved.

Assumptions and continuity equation. The following assumptions are realistic:

1. There is only one nonzero velocity component, namely that in the direction of flow, v_z . Thus, $v_r = v_\theta = 0$.
2. Gravity acts vertically downwards, so that $g_z = 0$.
3. The axial velocity is independent of the angular location; that is, $\partial v_z / \partial \theta = 0$.

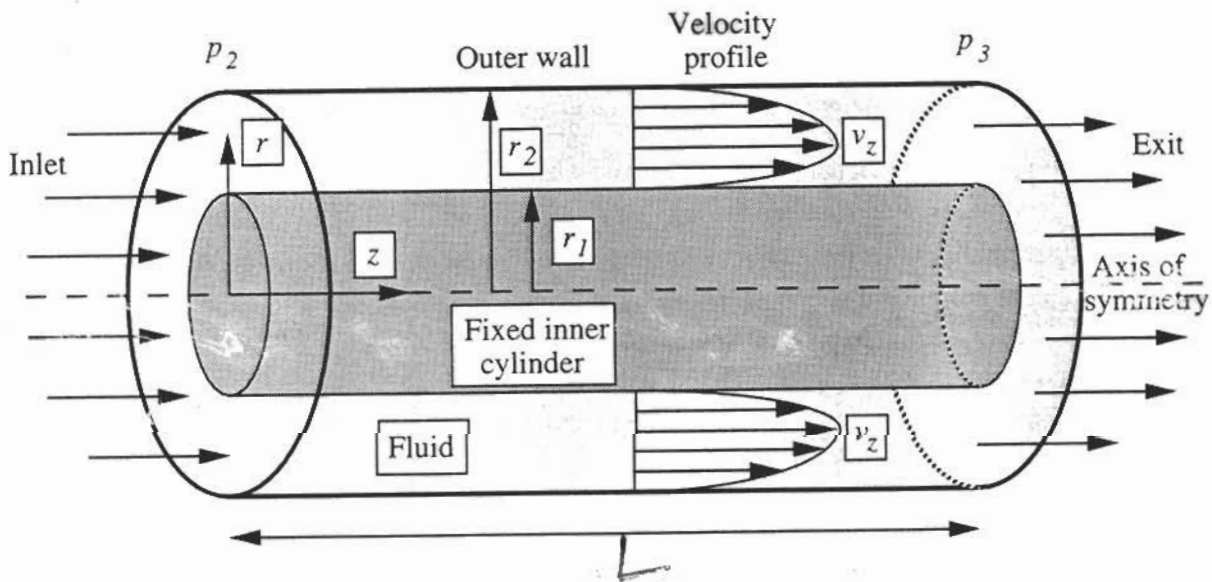


Fig. E6.5 Geometry for flow through an annular die.

Solution:

Continuity equation:
$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial(\rho r v_r)}{\partial r} + \frac{1}{r} \frac{\partial(\rho r v_\theta)}{\partial \theta} + \frac{\partial(\rho v_z)}{\partial z} = 0,$$

$$\Rightarrow \frac{\partial v_z}{\partial z} = 0, \quad v_z = f(z) \text{ also for axisymmetric flow}$$

$$v_z = f(\theta) \Rightarrow v_z = f(r) \text{ only.}$$

Navier-Stokes Equations:

$$v_r = v_\theta = 0 \quad , \quad \frac{\partial}{\partial \theta} (\text{any thing}) = 0 \quad \left(\begin{array}{l} \text{axisymmetric} \\ \text{problem} \end{array} \right)$$

v_z , and $v_z = f(r)$ only.

$$\begin{aligned} \rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) \\ = -\frac{\partial p}{\partial r} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (r v_r)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right] + \rho g_r, \end{aligned}$$

$$\begin{aligned} \rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r v_\theta}{r} + v_z \frac{\partial v_\theta}{\partial z} \right) \\ = -\frac{1}{r} \frac{\partial p}{\partial \theta} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (r v_\theta)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} + \frac{\partial^2 v_\theta}{\partial z^2} \right] + \rho g_\theta, \end{aligned}$$

$$\begin{aligned} \rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) \\ = -\frac{\partial p}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z. \end{aligned}$$

simplify: $0 = -\frac{\partial p}{\partial z} + \mu \left[\frac{1}{r} \frac{d}{dr} \left(r \frac{dv_z}{dr} \right) \right]$

pressure variation in z-direction is linear

$$\Rightarrow \frac{\partial p}{\partial z} = \frac{\Delta p}{L}$$

$$\Rightarrow \frac{1}{r} \frac{d}{dr} \left(r \frac{dv_z}{dr} \right) = \frac{\Delta p}{\mu L}$$

integrate twice:

$$v_z = \frac{\Delta p}{4\mu L} r^2 + C_1 \ln(r) + C_2$$

boundary conditions :

r = r1 v2 = 0 (no-slip BC)

r = r2 v2 = 0 (no-slip BC)

→ 0 = ΔP / (4μL) r1^2 + c1 ln(r1) + c2 (1)

0 = ΔP / (4μL) r2^2 + c1 ln(r2) + c2 (2)

(1) - (2) ⇒ ΔP / (4μL) (r1^2 - r2^2) + c1 ln(r1/r2) = 0

⇒ c1 = [ΔP / (4μL) (r2^2 - r1^2)] / ln(r1/r2)

substitute in (2) :

c2 = - ΔP / (4μL) r2^2 - [ΔP / (4μL) (r2^2 - r1^2)] / ln(r1/r2) ln(r2)

substitute c1 & c2 in velocity profile

⇒ v2 = ΔP / (4μL) [(r^2 - r2^2) + (r2^2 - r1^2) / ln(r1/r2) ln(r/r2)]

Volumetric flow rate

Q = ∫A v2 dA

$$Q = \int_0^{2\pi} \int_{r_1}^{r_2} v_z r dr d\theta$$

do it yourself

$$Q = \frac{\pi (r_2^2 - r_1^2)}{8\mu} \frac{\Delta P}{L} \left[\frac{r_2^2 - r_1^2}{\ln\left(\frac{r_2}{r_1}\right)} - (r_2^2 + r_1^2) \right]$$

Stress Tensor:

recall $v_r = v_\theta = 0$ $\frac{\partial}{\partial \theta} () = 0$

$v_z = f(r)$ only

$$\tau_{r\theta} = \tau_{\theta r} = \mu \left(r \frac{\partial}{\partial r} \left(\frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right),$$

$$\tau_{\theta z} = \tau_{z\theta} = \mu \left(\frac{\partial v_\theta}{\partial z} + \frac{1}{r} \frac{\partial v_z}{\partial \theta} \right),$$

$$\tau_{zr} = \tau_{rz} = \mu \left(\frac{\partial v_z}{\partial r} + \frac{\partial v_r}{\partial z} \right).$$

$$\sigma_{rr} = -p + 2\mu \frac{\partial v_r}{\partial r} - \frac{2}{3}\mu \nabla \cdot \mathbf{v},$$

$$\sigma_{\theta\theta} = -p + 2\mu \left(\frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r}{r} \right) - \frac{2}{3}\mu \nabla \cdot \mathbf{v},$$

$$\sigma_{zz} = -p + 2\mu \frac{\partial v_z}{\partial z} - \frac{2}{3}\mu \nabla \cdot \mathbf{v}.$$

$$\tau_{rz} = \tau_{zr} = \mu \frac{dv_z}{dr}$$

$$= \frac{\Delta P}{4L} \left[2r + \frac{r_2^2 - r_1^2}{\ln\left(\frac{r_1}{r_2}\right)} \frac{1}{r} \right]$$