

# Drag Force on Solid Particles in fluids

$$Re = \frac{\rho U_{\infty} D}{\mu}$$

Laminar flow	$Re < 1$	$C_D = \frac{24}{Re}$
Transition flow	$1 < Re < 1000$	$C_D = 18 Re^{-0.6}$
Turbulent flow	$Re > 1000$	$C_D = 0.44$

\* experimental data for the drag on a smooth sphere can be correlated in terms of two dimensionless groups

$$C_D = \frac{F_D / A_p}{\frac{1}{2} \rho U_{\infty}^2} \quad \text{drag Coefficient}$$

$$Re = \frac{\rho U_{\infty} D}{\mu}$$

$$\boxed{F_D = 3\pi\mu U_{\infty} D} \quad \text{only for laminar flow}$$

\* for a constant sphere travelling at its terminal velocity

$$F_D = \frac{\pi}{6} D^3 (\rho_s - \rho_f) g$$

$$\therefore C_D = \frac{4}{3} \frac{gD}{U_t^2} * \frac{\rho_s - \rho_f}{\rho_f}$$