



King Fahad University of Petroleum and Minerals
Construction Engineering and Management Department

CONSTRUCTION QUALITY ASSURANCE

CEM-515

Project Paper

Project Title: Reactor Improvement Level Control

Prepared To: Dr.
ABDULAZIZ A. BUBSHAIT

Abdulrahman Al-Ghamdi (ID# 230143)

4 Decembers 2004

REACTOR IMPROVEMENT LEVEL CONTROL

TABLE OF CONTENTS

- ☛ Abstract
- ☛ Introduction
- ☛ Phase 1: Define the quality issue
- ☛ Phase 2: Understand and define the process
- ☛ Phase 3: Select improvement opportunities
- ☛ Phase 4: Analyze the improvement opportunities
- ☛ Phase 5: Take action
- ☛ Phase 6: Check results
- ☛ Phase 7: Implement the improvement
- ☛ Phase 8: Monitor results
- ☛ Conclusion
- ☛ References

REACTOR IMPROVEMENT LEVEL CONTROL

ABSTRACT

In this paper, the eight phases of the customer-driven project management improvement methodology are used to solve the unexpected process shutdowns during the operation of the Plant due to the quality of the level control that used on the Reactor.

INTRODUCTION

Chemical plants must operate under known and specified conditions. There are several reasons why this is so, formal safety and environmental constraints must not be violated. Concern for safety is paramount in designing a chemical plant and its control systems. Ideally a process design should be 'intrinsically safe', that is, and plant and equipment should be such so that any deviation, such as an increase in reactor pressure, will itself change operating conditions so that it is rapidly removed. Plants are expensive and intended to make money. Final products must meet customer specifications. Otherwise, they will be unsaleable. Conversely the manufacture of products not meeting the specifications will involve unnecessary cost. The majority of control loops in a plant control system are associated with operability. Specific flow rates have to be set, levels in Reactor maintained and chosen operating temperatures for reactors and other equipment achieved. The top level of process control, what we will refer to as the *strategic* control level, is thus concerned with achieving the appropriate values principally of: production rate, product quality, and energy economy. The feedback level control system seeks to bring the measured quantity to its required value or setpoint.

Phase one Define the Quality issue

The mission of this Project is to improve the Reactor level control measurement system in terms of quality. It is desired that improve the reliability of this system will help and avoid unexpected process shutdowns during the operation of the Plant. Polymerization reactor is fluidized bed reactor; it used to produce polyethylene resin (granules). This reactor is operated at 21 Bar and temperature ranges from 80–100 deg C. The bed level should be controlled between 14 & 17 m because of process impact if it is out of this range. The Customer (Operation) expectation to have a good system for the reactor level control

REACTOR IMPROVEMENT LEVEL CONTROL

Phase two understand and define the Process

This reactor has two type of controlling for the Bed Level. The first system is purge type DP transmitters. The Purge taps system works well in terms of measurement and control, however the most problems in this system reliability and maintenance. The purge taps are frequently getting plugged and need to be purged and oftentimes drilled. Drilling is a very critical operation in term of safety. The second system is Remote seal differential pressure transmitter was installed on the reactor for monitoring the bed level in the reactor as a back up to the purge type DP transmitters for reactor level and control. Since the remote seal type transmitters had installed, the reading of these transmitters are swing, not accuracy and not matching with the Purge type due to the ambient temperature variation. This problem could result in plant shutdown and production rate reduction. I followed the improvement methodology and arrived at a conclusion in which the problem would be resolved at lower cost and without jeopardizing the quality of the work and/or impacting the performance of the system.

REACTOR IMPROVEMENT LEVEL CONTROL

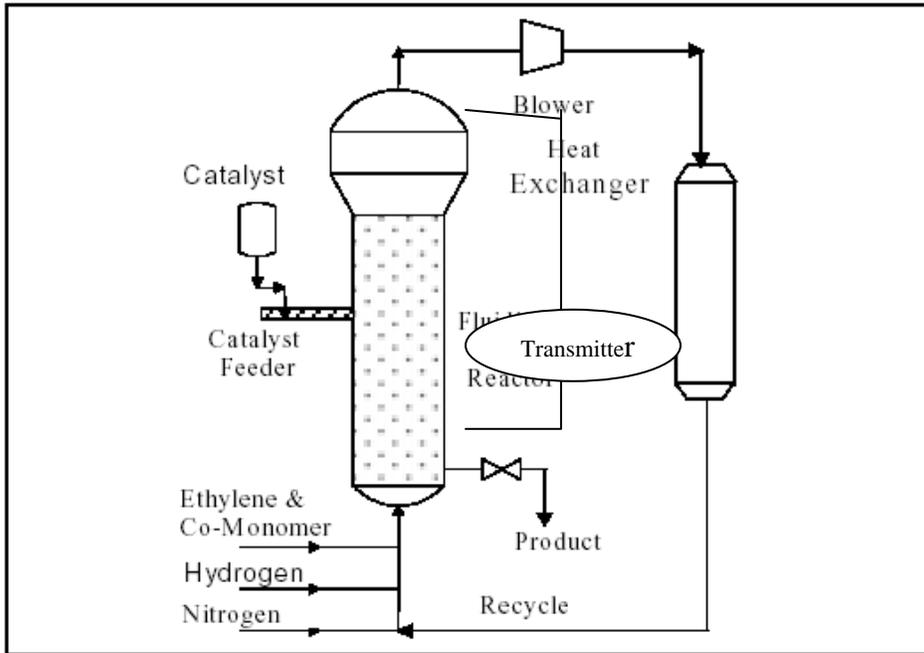


Fig1: Reactor design and configuration

Phase three Select Improvement opportunities

It not essays to select any type of measurement form the market .I came up with different solutions to these problems. However, I did feasibility study with different instrument, Process Engineers and vender, this feasibility was survey to select the best solution for improvement the Reactor bed Level Measurement for both systems.

During this phase, different proposals evaluated to improve the remote seal and the purge taps. I went further and looked for other available technology and support in the market for one of the two systems. Normally this phase should have a creative session to generate ideas. These ideas should be listed and captured. So, I generated different ideas during the creative phase. I did feasibility study by sent these ideas to different Engineers and vendor for ranking the ideas; I had very good result with the feasibility study. The Engineers were very open in accepting others ideas which helps me to come up with 5. All these ideas were studied in-depth and two ideas were selected to be the best among others ideas. Ideas and suggestions generated by the Engineers are listed below:

REACTOR IMPROVEMENT LEVEL CONTROL

No	Ideas/Suggestions	Ranking
1	Improve the purge tap DP Measurement by install purge valves near the affected transmitter to keep the leads swept clean	4
2	To reduce the error caused by temperature swing, both the capillary lengths needs to be revisit and reduced, if possible.	2
3	Use Model 3051S electronic seal system Ultra Scalable DP transmitter with Remote seal to get better performance	2
4	Install camera with light	3
5	Install radioactive sources and detector	2

Ranking: (Not acceptable = 0, Poor =1, Fair = 2, Good=3, Very Good=4, Excellent =5)

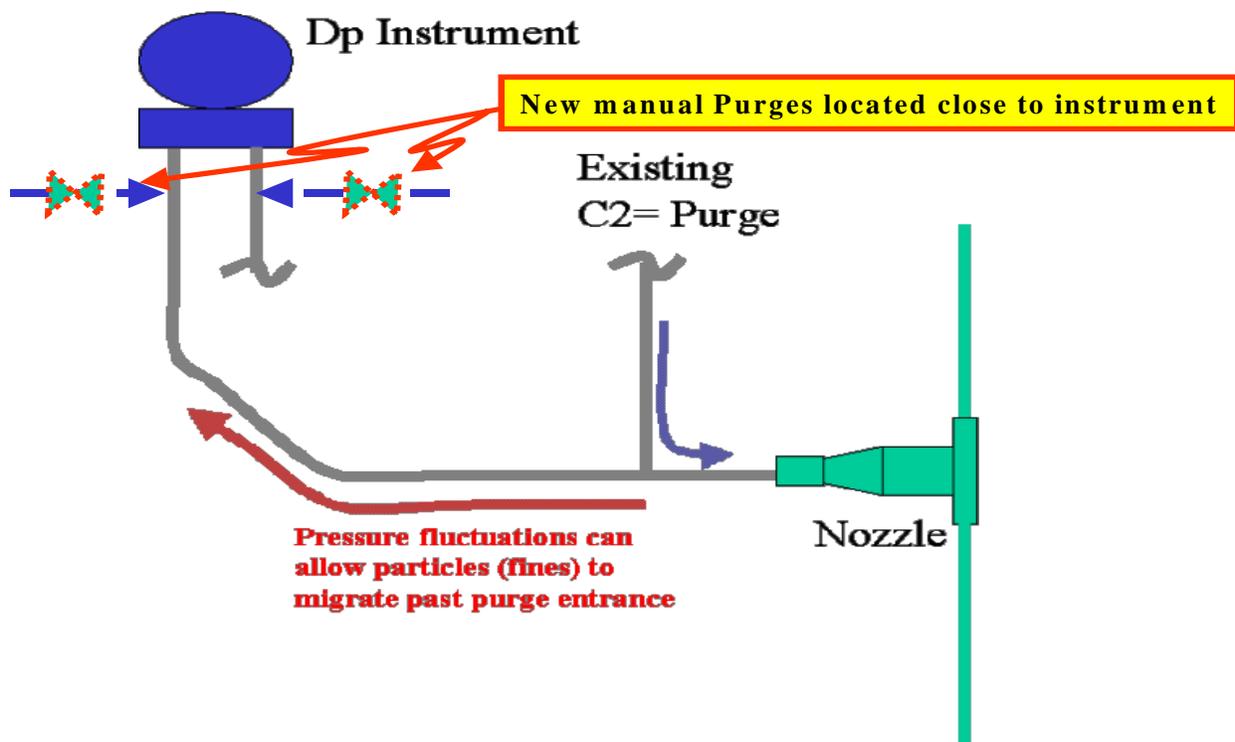
As a result of the creative session, the team selected the highest ranked ideas for further development and evaluation. The selected ideas are listed below:

- I. Improve the purge tap DP Measurement by install purge valves near the affected transmitter to keep the leads swept clean.
- II. . Install camera with light
- III. Install radioactive sources and detector

REACTOR IMPROVEMENT LEVEL CONTROL

Improve the purge tap DP Measurement by install purge valves near the affected transmitter to keep the leads swept clean.

The ethylene purge is also located very close the nozzle. The distance between the entry point of the purge and the actual instrument lead is very long (leaving large unpurged pocket). Pressure fluctuations in the C2 purge header and/or reactor can allow resin fines to travel (intermittently) backwards in the tubing past the purge point (see sketch below). When this happens, the tubing becomes partially fouled and errors are seen in the Dp signals. Fluctuations in pressure during manual blowback often dislodge the material and it eventually makes it way to the purged portion of the tubing and flows back in to the reactor. Often this material remains lodged in the tubing leads and the taps must be vented or drilled. So, to mitigate this issue we will install purge valves near the affected transmitter to keep the leads swept clean. The existing purge lines that go directly to the nozzle can be left intact but manually blocked. When drilling or excessive purge is required, the existing manual block can then be utilized (opened). The concept & design is shown in the sketch below. This will improve the quality of the Existing purge tap.



REACTOR IMPROVEMENT LEVEL CONTROL

Install camera with light.

Function: The Canty Vision and Vector systems provide a unique ability to view and control difficult reactor processes allowing operators to maximize throughput, detect and eradicate foaming and to document process events anytime during the duration of the reaction. In order to accomplish process control a quality image of the reactor internals is required. The Canty Vision system is ideally suited for this purpose due to its rugged construction and patented design features that combine to overcome process variables that would otherwise prevent a quality image capture. The Canty Vision system provides illumination and video function through a single port. This design optimizes the viewing area resolution by directing illumination to the reactor area that the camera “sees”. This also eliminates the need for multiple ports, which can be expensive and valuable for process considerations. The fused glass design of the lens also provides for high pressure, high temperature performance capabilities.

The Canty system is completed with the optional Jet Spray Ring, which is used to provide cleaning fluid to the lens system. In many reactors splashing, vapor condensation or other process deposits on the lens can obstruct the view of the camera. With the Jet Spray Ring, cleaning agents can be introduced to the front of the lens to remove any obstructing materials and prevent them from condensing onto the lens.

Once a process image is obtained, the Vector NT system can provide the control features to maximize process efficiency. The system operates as does the human eye – by differentiating light intensities at object boundaries. Detecting the level in a reactor then becomes a straightforward analysis of the image for the interface of fluid (solid) and the reactor wall. Because the process sensing is done visually, the system can provide control on agitated reactors with accuracy. In addition, the system can track level as product changes phase (foams) and can provide immediate detection of the occurrence of foam so it can be eliminated.

The image from a single camera can be analyzed several times for different data – level, foam and color (Vector can also provide turbidity, %solids, particle size with the appropriate companion hardware). Finally, because the system is visual there is a constant, real time verification on the monitor for the operator to use as a check.

REACTOR IMPROVEMENT LEVEL CONTROL

Equipment: Cauty Vision System – Camera/Light combination unit, EXP/WP ratings, B/W or Color, standard flange mount (other available), stainless steel, hastelloy wetted materials standard, various view angles available.

Cauty Vector NT – NT based image processing unit with up to 4 camera input, 8 channel 4–20 mA output, modem for factory support, Excel based data output, user friendly operator interface.

REACTOR IMPROVEMENT LEVEL CONTROL

CANTY CAMERA SYSTEMS

PROCESS TECHNOLOGY



HOW IT WORKS

J.M. Canty cameras are patented systems designed to illuminate and view inside a pressure or process vessel through a single connection. There is no need for multiple vessel ports. Canty supplies an integrally mounted camera and lighting system (optional) in a connection as small as a 2" NPT. The industry standard video output can be displayed on a video monitor in the comforts of a control room, or recorded on any VCR. A standard video monitor or TV with video input may be used to display the image.

CANTY LIGHTS MAKE IT POSSIBLE

The key to Canty Camera/Light combination systems is the Canty light. Canty uses fiber optic light guides to focus cool, effective light into a process vessel or area. Cool light eliminates product bake-over on the viewing window. Fiber optic light guides have been specifically designed to work in conjunction with cool light to maximize the light transmission into the vessel. The resulting live, remote video image from this illumination is unparalleled!

THE COMPLETE PACKAGE

Canty can meet all your needs! Included as standard equipment on every camera system are power supplies, a high resolution B & W or color CCD camera, pre-focused lens and WP, IP66, explosion proof or flame proof enclosure. What's more – all wiring and maintenance are external. Many optional monitors, recording and control options are available. All cameras can be easily integrated with a Canty Vector System for various process measuring and control functions such as non-contact level control, particle sizing, etc. Please consult the factory for details.

APPLICATIONS

- ❑ Polymers – Verify empty, monitor level
- ❑ Crystallizers – Liquid and foam level
- ❑ Fermentors – Liquid and foam level
- ❑ High purity pharmaceutical applications
- ❑ Toxic Material – Remote viewing
- ❑ Foam and Fluid Level monitoring in:
 - Shredders Hoppers
 - Nutsch Filters Latex Applications
 - Strippers Pressure Vessels

FEATURES

- ❑ FM, CSA and approvals to CENELEC on various models. World wide approval!
- ❑ 10,000 PSI ratings are available
- ❑ Up to 2000° F capabilities
- ❑ 2" NPT, 3" flange and larger, 3" tri-clamp® and larger connections are available.
- ❑ High resolution CCD cameras – available in B&W and color, NTSC and PAL
- ❑ Remotely view your process from the comforts of a control room
- ❑ Single nozzle viewing/illuminating (with light)
- ❑ Remote light dimming options
- ❑ Spray rings are available to keep your window clean

SPECIFICATIONS

CCD Sensor:	1/2" format. 500(H) x 480(V) typ.
Sensitivity:	Available from .01 lux usable picture (low light B&W). 3 lux is typical (color). Varies with model.
Video Output:	1.0 V p-p, 75 Ω typ.
Ambient Temp:	- 30°C to 50°C
Current Req.:	500 mA typical
Cable:	RG 59/U, 75 Ω coaxial cable suitable for CCTV applications
Environmental ratings:	NEMA 4, IP66, Explosion proof (Class 1, Div. 1, Groups B, C & D, Class II, Div. 1, Groups E, F & G) or Flameproof EEx d IIC

OPTIONS

- Vector System - level/foam control, volume control, in-line particle sizing, color analysis
- Time/date generators – overlay time and date stamp onto video picture
- Data overlay – overlay pH, temp, pressure, etc. onto video picture
- Fiber Optic Link – replaces coaxial cable, need for conduit

CANTY

PROCESS TECHNOLOGY

JET SPRAY RING



JET SPRAY RING MODELS

Open Channel

Most popular spray ring model. For use with Fuseview™ flat gasket, non-insertion style lights and cameras. Recommended for use with full-faced gaskets. Fluid distribution channel is accessible.

Closed Channel

For use with Fuseview™ flat gasket, non-insertion style lights and cameras. Fluid distribution channel is not accessible.

Closed Channel Insertion

Use with any CANTY insertion camera or light.

UNIQUE DESIGN

The Cauty Jet Spray Ring generates a high pressure vortex rinsing action to remove tough deposits from sightglasses, lights and vision systems.

The Jet Spray Ring accepts a rinsing/cleaning solution and distributes the pressurized material through the specially designed rinse ports. These rinse ports have been engineered to provide maximum cleaning power in a compact package. The Jet cleaning action expels all debris from the sightglass, providing an exceptional view into the process.

The Jet Spray Ring may be used for constant preventive or instantaneous blast-off cleaning. As a suggestion, cleaning may be timed for 5 seconds every hour, or tied in with normal CIP (Clean in Place). Any low viscosity fluid compatible with your process may be used. Common cleaning agents for powder service include air and nitrogen, while common liquid service agents include water or solvents.

APPLICATIONS

- Process Vessels
- Laboratory Reactors
- Research Vessels
- Dryers
- Pressure Chambers
- Incinerators
- Many, many more!

FEATURES

- Materials: Stainless Steel
 Hastelloy
 Aluminum
 Titanium
 Monel
 Inconel
 Teflon ®
- Mounting: ANSI and DIN sizes
- Pressures: 150 PSI, 16 bar
 Pressures up to 5000 PSI are
 available on certain models
- Sizes: 1.5" ANSI and larger
 40 mm DIN and larger

Please consult the factory or your local representative for custom applications.

JET SPRAY RING - US SPACE PROGRAM ORIENTATION

The Jet Spray Ring was originally designed to eliminate bothersome PVC build-up on sightglasses and used in the manufacture of heat shield tile epoxy for the US space shuttle program. Since it's original conception, the spray ring has been used on many applications in the pharmaceutical, chemical, petro-chemical and dairy industries.

JM CANTY INC.

Buffalo, NY USA
Ph:(716)625-4227
Fax:(716)625-4228

JM CANTY LTD.

Dublin, Ireland
Ph:(353)(01)459-8808
Fax:(353)(01)462-5133

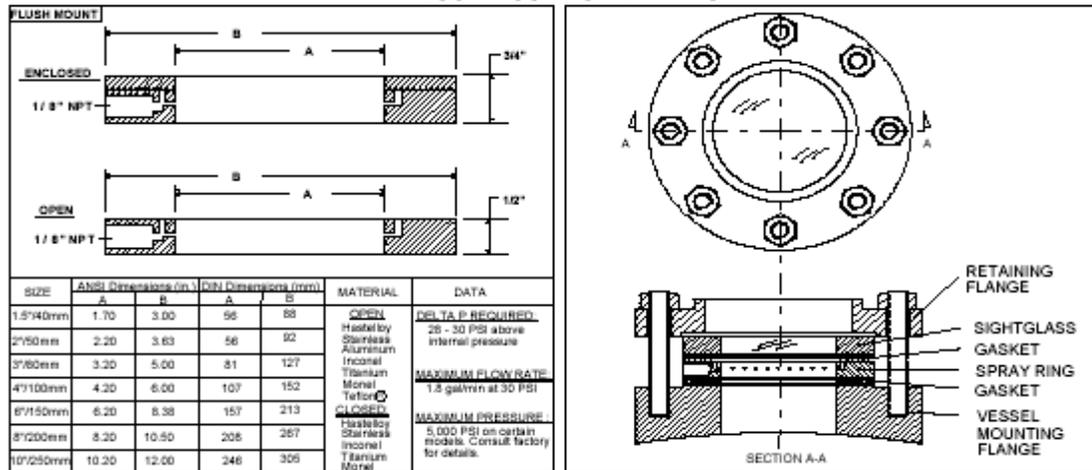
sales@jmcanty.com

Represented by:



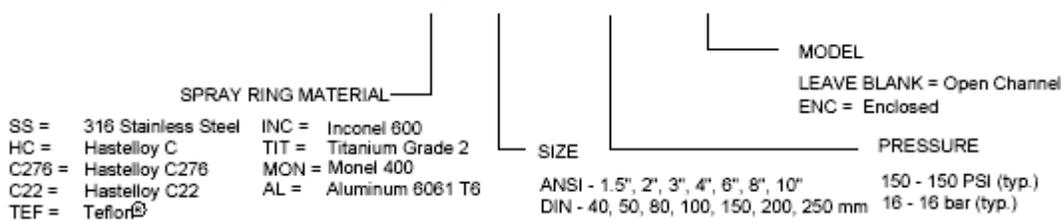
REACTOR IMPROVEMENT LEVEL CONTROL

FLUSH MOUNT SPRAY RING

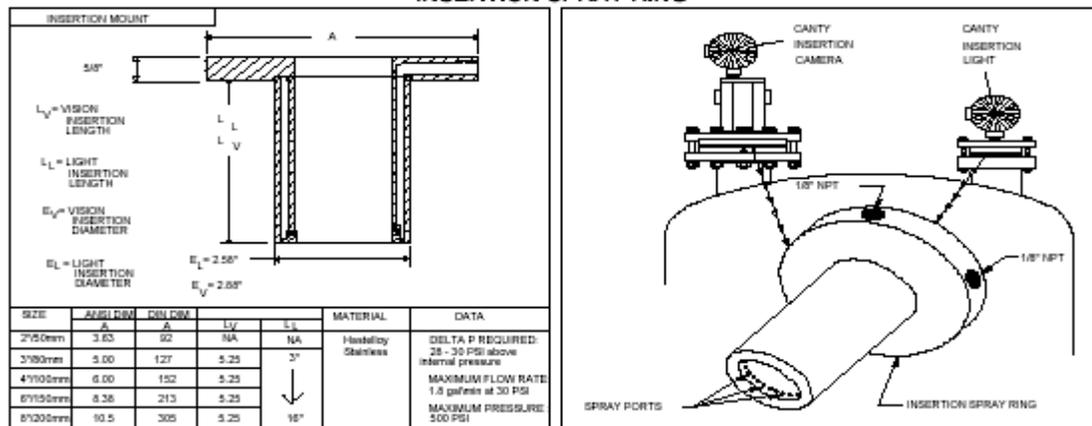


HOW TO ORDER: Select the appropriate symbols and build a model number as shown:

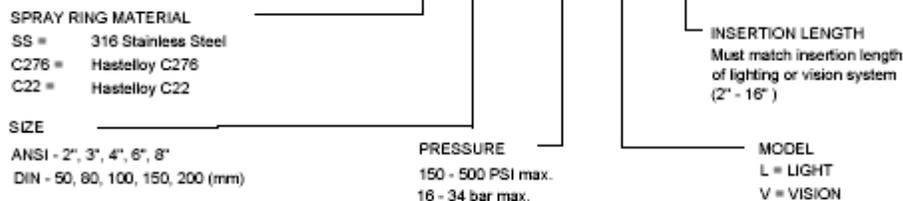
EXAMPLE: **SS - 4 - SR150 - ENC**



INSERTION SPRAY RING



EXAMPLE: **SS - 4 - SR150 - L - 6INS**



Teflon is a registered trademark of the Dupont Corporation.
Document # 98A4727 Rev. 0103096

CANTY

PROCESS TECHNOLOGY

COMPUTER SYSTEMS - VECTOR/VECTOR DESK



THE CANTY ADVANTAGE

The Vector System uses the live video data from a Canty Vision System to measure and control your process parameters. The Vector System converts the video from a Canty camera system into a matrix of pixels at 30 frames/sec. (with a single input) to a resolution of over 256 shades of gray (B&W systems) or over 16 million colors (color systems). Each input is analyzed by the specified software to perform the desired process control functions. Any software package can be selected with any camera (except particle size distribution - contact factory).

OUTPUT OPTIONS

The Vector System has various outputs available, including numerous user interface menus and network connectivity to standard 4-20 mA current loop devices. Particle sizing software packages also feature distribution graphs and histogram outputs. All Vector models are fully compatible with all of the standard Microsoft communications protocols. Canty Offers Custom output packages if needed.

PARTICLE SIZING

All particle sizing packages are provided with a Spreadsheet application. Measured particle data is written into a standard spreadsheet format, where it is available to the user for analysis. Canty provides many standard output tables and graphs. Custom tables and graphs can easily be created using the application or data can be converted to other supported file formats.

SOFTWARE OPTIONS

- Level / Volume Control
- Foam Detection
- In-line Particle Sizing -1D, 2D analysis
- Lab Particle Sizing
- Conveyor-Flow, Belt Breaking Applications
- Alignment, Cleanliness Applications
- Color Analysis
- Baking Control
- Size and Shape Analysis
- Glass Glob / Float Glass Analysis
- Percent Solids, Opacity, Turbidity
- Black Speck Detection
- Custom Applications - Consult Factory

FEATURES

- Microsoft Windows based operating system
- Options for Multiple Video Inputs on the 19" Vector system.
- Ethernet connectivity to 4-20 mA devices
- Internal modem for technical support and remote user interfacing
- Multiple software process control packages
- Network Card
- Images may be recorded and saved to the hard disk for future measurements or for archival purposes.
- Industrial microprocessor
- Filtered multi-fan cooling system

SPECIFICATIONS

User Interface:	MS Windows based OS
Voltage:	120 Volt AC, 60 Hz (U.S.) 230 V AC, 50 Hz (Europe)
Video Input:	Available models include: EIA (B&W - U.S. format) NTSC (Color - U.S. format) CCIR (B&W - European format) PAL - (Color - European format)
Approvals:	CE marking for Europe (CCIR,PAL systems)
Power Req:	400 VA typical
Mounting:	Compact Transmitter Chassis
Modem :	Internal (standard)
Imaging:	On board imaging processor
Network Int.:	Ethernet

REACTOR IMPROVEMENT LEVEL CONTROL

Ordering Information

HOW TO ORDER: Select the appropriate symbols and build a model number as shown:

EXAMPLE:

VCB3500-LIC

VISION SYSTEM FORMAT

- C - U.S. Format
- P - European Format

VIDEO INPUT

- C - Color
- B - Black & White

OPERATING SYSTEM

- 3 - Windows

MOUNTING CONFIGURATION

- 4 - Vector 19" Rack Mount Chasis
- 5 - Vector Desk Mount Chasis

SOFTWARE PACKAGE

- LIC - Level/Edge & Intensity
- PS - Particle Size & Speck Detection
- EPS - Bead Size

mA OUTPUT OPTIONS

- 0 - No 4-20mA Outputs
- 1 - 8 Channel 4-20mA Outputs*
- 2 - 16 Channel 4-20mA Outputs*

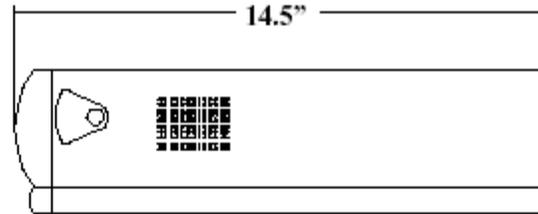
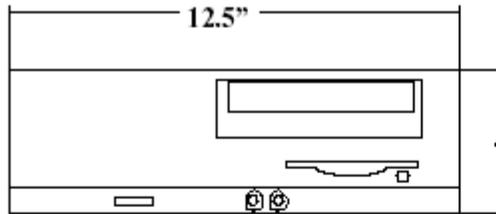
MULTIPLEXER OPTIONS

- 0 - None (One camera input)
- 1 - Multiplexer (Up to 4 Video Inputs)*
- 2 - Multiplexer (Up to 8 Video Inputs)*
- 3 - Multiplexer (Up to 12 Video Inputs)*

* This option is for the Vector 19" Rack Mount Chasis only

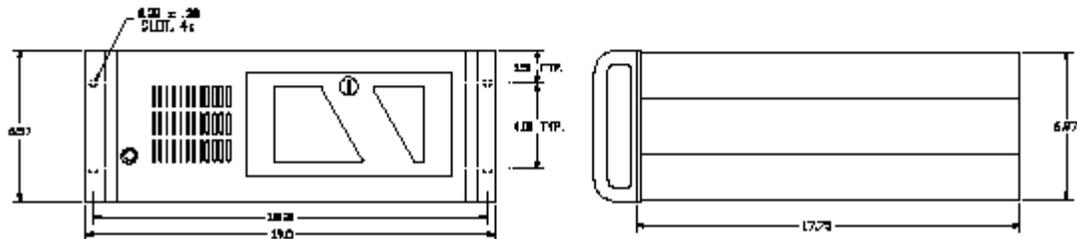
** User supplies SVGA monitor and keyboard for all systems

TRANSMITTER CHASIS



The transmitter Vector Desk package is the most compact (weighing in at approximately 15lbs) and the most economical unit available. While the Vector is the most economical rack mount available. Both transmitter packages require the following equipment that must be supplied by the user for stand alone operation except for the Mounting Cabinet which is only for the 19" rack mount Vector.

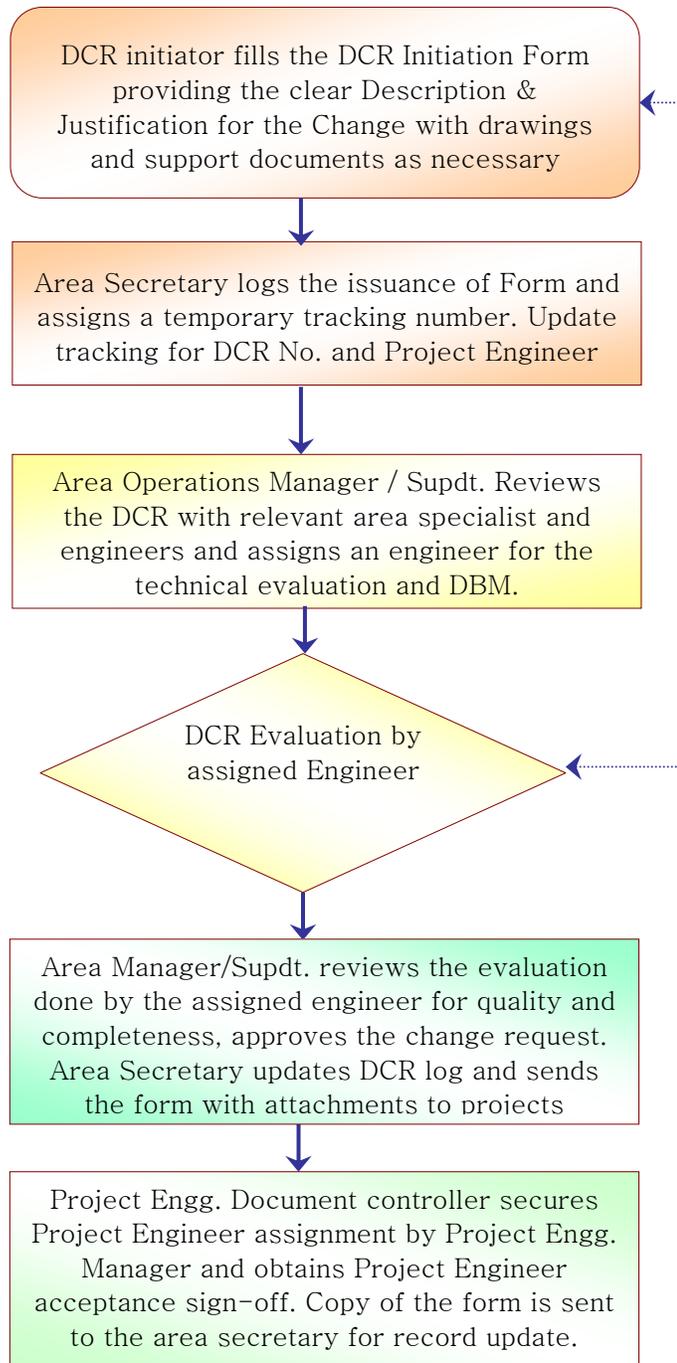
- SVGA monitor
- Standard keyboard
- A mouse is included with each transmitter Vector Desk system
- Mounting cabinet (19" rack enclosure is recommended)



REACTOR IMPROVEMENT LEVEL CONTROL

Phase Five Tack Action

DCR Initiation Form Flow Chart



REACTOR IMPROVEMENT LEVEL CONTROL

Phase 6: Check results

Phase 7: Implement the improvement

Phase 8: Monitor results

REACTOR IMPROVEMENT LEVEL CONTROL

References

Dear Mr. Abdulrahman,

My apologies. I could not send you the reply yesterday because my computer crashed and it took several hours to get it back online.

further to my detailed discussions with Emerson technical support manager regarding the Fluidized bed Reactor powder level application at KEMYA and following are the details and suggestions

1. For Purge Type DP Level measurement, the purge connections should be near to the process tapping point. The purging medium should not flow thro the transmitter. The back pressure created for level measurement should be stagnant not flow thro.

2. It is recommended to stay with Purge type DP level measurement due to the following reasons.

a) 3051S DP transmitter with impulse line plugging Diagnostics and Fieldbus Host to detect & report line plugging can not be used for level measurements. At present this facility is available only for flow applications.

b) Due to high Ambient temperature variations, Remote seal transmitters may cause additional measurement error and it could not be eliminated due to the application requirements of long capillary. purge type measurements do not have this temperature effect error in measurement.

c) Electronic seal system is also not recommended due to 10 to 14% measurement error and Fieldbus host requirements also the system is not yet tested for this kind of application.

3. Due to the above reasons, purge type Dp level measurement may be the right solution with additional accessories (Automatic Blow back system) to improve the performance of the system and reduce frequent line plugging problem.

4. The over all accuracy of the purge Type transmitter can be improved by using Model 3051S ultra Scalable DP Transmitter (0.04% accuracy, 10 year stability, 12 year warranty Transmitter).

trust this clarify all your questions and should you require any further details, please let us know.

thanks & best regards

Kumar.

PLEASE CONFIRM RECEIPT OF THIS MAIL.

REACTOR IMPROVEMENT LEVEL CONTROL

Lakshman Kumar
Manager – Rosemount Measurement Systems
Saudi Fal Co. Ltd., (EMERSON Process Management)
P.O.Box 3070, Al-Khobar 31952, Saudi Arabia.
Tel : +966 3 857 3157 Ext. 146
Fax : +966 3 857 8491
Mobile : 00966 504821094
e-mail : kumar.lakshman@saudifal.com.sa
website : <http://www.saudifal.com.sa/>

[Emerson Process Management <http://www.emersonprocess.com>](http://www.emersonprocess.com), an Emerson business, is a leader in helping businesses automate their production, processing and distribution in the chemical, oil and gas, refining, pulp and paper, power, food and beverage, pharmaceutical and other industries. A division of Emerson, Rosemount Inc. is a global leader in high-precision pressure, temperature, level, and flow instrumentation. Rosemount's best-in-class technology and expertise play a key role in Emerson's combining of superior products and technology with industry-specific engineering, consulting, project management and maintenance services.

Emerson Process include: Fisher® <http://www.fisher.com>, Rosemount® <http://www.rosemount.com>, Intellution® <http://www.intellution.com>, Micro Motion® <http://www.micromotion.com>, Daniel <http://www.daniel.com>, Westinghouse Process Control <http://www.westinghousepc.com>, PlantWeb® <http://www.plantweb.com>, DeltaV <http://www.easydeltav.com> and AMS <http://www.emersonprocess.com/ams>.

Abdulrahman Al-Ghamdi

Senior.Instrument & PLC Engr.

Al-Jubail Petrochemical Co. (KEMYA)

Phone: 03 357 6539

Fax: 03 357 6058

mobile 055911014

E-mail: <mailto:ghamdiaa2@kemya.sabic.com>

REACTOR IMPROVEMENT LEVEL CONTROL

-----Original Message-----

From: GHAMDI AL-, Abdulrahman A
Sent: Tuesday, June 08, 2004 11:52 AM
To: 'KUMAR LAKSHMAN [Saudi Fal/Al-Khobar]'
Subject: RE: Level Transmitters in Fluidized Bed Reactor-R0401

Kumar Please find the attached files for your action

Best regard

Abdulrahman Al-Ghamdi

Senior.Instrument & PLC Engr.

Al-Jubail Petrochemical Co. (KEMYA)

Phone: 03 357 6539

Fax: 03 357 6058

mobile 055911014

E-mail: <mailto:ghamdiala2@kemya.sabic.com>

-----Original Message-----

From: KUMAR LAKSHMAN [Saudi Fal/Al-Khobar]
[mailto:kumar.lakshman@saudifal.com.sa]
Sent: Wednesday, April 21, 2004 9:42 AM
To: GHAMDI AL-, Abdulrahman A
Cc: P. SIVA; Suresh V [FRCO/DUB] (E-mail); Pattabhiraman Ganesh
[FRCO/DUB] (E-mail)
Subject: Level Transmitters in Fluidized Bed Reactor-R0401

Dear Abdulrahman,

This is in response to our site visit and discussions regarding the Level transmitters installed on the Reactor R0401 for Fluidized Bed Level Measurements. We thank you for your excellent support and the details provided to study this application. We carefully gone thro the application details and the documents provided by you and following are our findings.

Objective:

1. Reduce error on level measurement introduced by Remote seals due to ambient temperature changes.

REACTOR IMPROVEMENT LEVEL CONTROL

2. Increase response time.
3. Increase reliability of the measurement by removing impulse line chocking.

1. Electronic seal System:

We have studied the possibility of introducing the Latest Rosemount 3051S Electronic seal System for this application. Though it eliminates the temperature effects of the capillary, but the over all % of error in level measurement is not better than the Standard remote seal for this particular application. Hence we do not recommend this system for this application.

2. Standard Remote seal Smart DP Transmitter with capillary:

We understand the main concern on this application is swinging of ambient temperature causes the measurement error. Measurement accuracy and reliability may be improved by the following methods.

1. Shorten the capillary.... Study the possibility of reducing the capillary length to the minimum.
2. Insulate and electric heat trace the capillaries to keep constant temperature of the capillary fill fluid.
3. Increase the seal diaphragm size from 2" to 3" to get better performance.
4. Use Model 3051S Ultra Scalable DP transmitter with Remote seal to get better performance.

find attached the performance calculations of the Model 3051S DP remote seal transmitter for this application.

trust the above details are sufficient for your immediate purpose to study and conclude.

Should you require any further details, please let us know.

thanks & best regards

Kumar

Lakshman Kumar
Manager – Rosemount Measurement Systems
Saudi Fal Co. Ltd., (EMERSON Process Management)
P.O.Box 3070, Al-Khobar 31952, Saudi Arabia.

REACTOR IMPROVEMENT LEVEL CONTROL

Tel : +966 3 857 3157 Ext. 146
Fax : +966 3 857 8491
Mobile : 00966 5 4821094
e-mail : kumar.lakshman@saudifal.com.sa
website : <http://www.saudifal.com.sa/>

[Emerson Process Management <http://www.emersonprocess.com>](http://www.emersonprocess.com), an Emerson business, is a leader in helping businesses automate their production, processing and distribution in the chemical, oil and gas, refining, pulp and paper, power, food and beverage, pharmaceutical and other industries. A division of Emerson, Rosemount Inc. is a global leader in high-precision pressure, temperature, level, and flow instrumentation. Rosemount's best-in-class technology and expertise play a key role in Emerson's combining of superior products and technology with industry-specific engineering, consulting, project management and maintenance services.

Emerson Process include: Fisher® [<http://www.fisher.com>](http://www.fisher.com), Rosemount® [<http://www.rosemount.com>](http://www.rosemount.com), Intellution® [<http://www.intellution.com>](http://www.intellution.com), Micro Motion® [<http://www.micromotion.com>](http://www.micromotion.com), Daniel [<http://www.daniel.com>](http://www.daniel.com), Westinghouse Process Control [<http://www.westinghousepc.com>](http://www.westinghousepc.com), PlantWeb® [<http://www.plantweb.com>](http://www.plantweb.com), DeltaV [<http://www.easydeltav.com>](http://www.easydeltav.com) and AMS [<http://www.emersonprocess.com/ams>](http://www.emersonprocess.com/ams).

Dear Abdulrahman,

This is in response to our site visit and discussions regarding the Level transmitters installed on the Reactor R0401 for Fluidized Bed Level Measurements. We thank you for your excellent support and the details provided to study this application. We carefully gone thro the application details and the documents provided by you and following are our findings.

Objective:

1. Reduce error on level measurement introduced by Remote seals due to ambient temperature changes.
2. Increase response time.
3. Increase reliability of the measurement by removing impulse line chocking.

1. Electronic seal System:

We have studied the possibility of introducing the Latest Rosemount 3051S Electronic seal System for this application. Though it eliminates the temperature effects of the capillary, but the over all % of error in level measurement is not better than the Standard remote seal for this particular application. Hence we do not recommend this system for this application.

2. Standard Remote seal Smart DP Transmitter with capillary:

We understand the main concern on this application is swinging of ambient temperature causes the measurement error. Measurement accuracy and reliability may be improved by the following methods.

1. Shorten the capillary.... Study the possibility of reducing the capillary length to the minimum.

REACTOR IMPROVEMENT LEVEL CONTROL

2. Insulate and electric heat trace the capillaries to keep constant temperature of the capillary fill fluid.
3. Increase the seal diaphragm size from 2" to 3" to get better performance.
4. Use Model 3051S Ultra Scalable DP transmitter with Remote seal to get better performance.

find attached the performance calculations of the Model 3051S DP remote seal transmitter for this application.

trust the above details are sufficient for your immediate purpose to study and conclude.

Should you require any further details, please let us know.

thanks & best regards

Kumar

Lakshman Kumar

Manager – Rosemount Measurement Systems

Saudi Fal Co. Ltd., (EMERSON Process Management)

P.O.Box 3070, Al-Khobar 31952, Saudi Arabia.

Tel : +966 3 857 3157 Ext. 146

Fax : +966 3 857 8491

Mobile : 00966 5 4821094

e-mail : kumar.lakshman@saudifal.com.sa

website : <http://www.saudifal.com.sa/>

Emerson Process Management <http://www.emersonprocess.com>, an Emerson business, is a leader in helping businesses automate their production, processing and distribution in the chemical, oil and gas, refining, pulp and paper, power, food and beverage, pharmaceutical and other industries. A division of Emerson, Rosemount Inc. is a global leader in high-precision pressure, temperature, level, and flow instrumentation. Rosemount's best-in-class technology and expertise play a key role in Emerson's combining of superior products and technology with industry-specific engineering, consulting, project management and maintenance services.

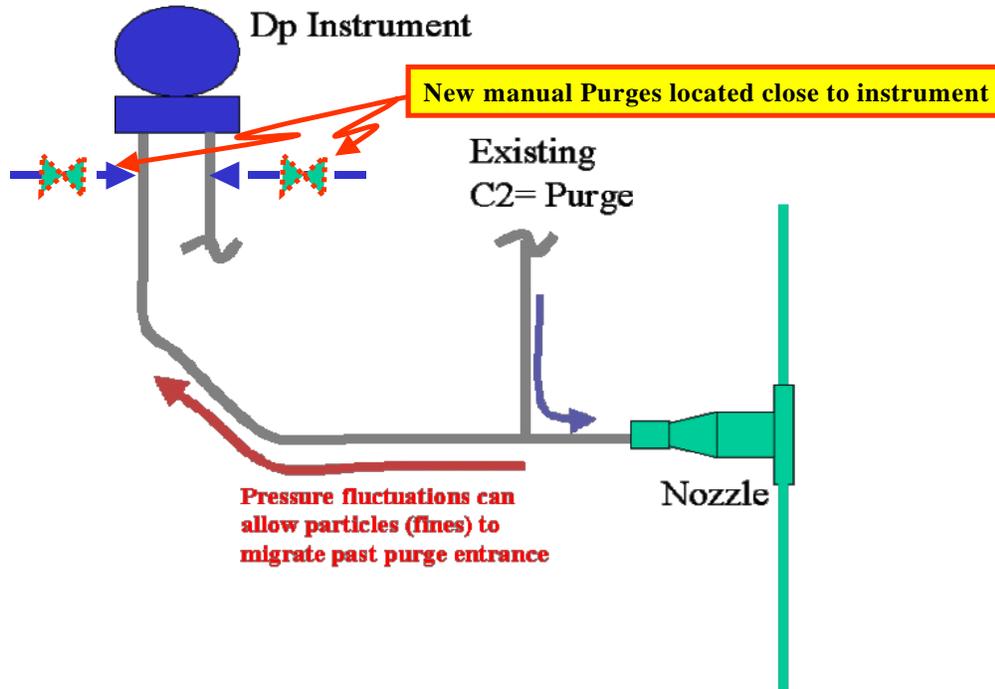
Emerson Process include: Fisher® <http://www.fisher.com>, Rosemount® <http://www.rosemount.com>, Intellution® <http://www.intellution.com>, Micro Motion® <http://www.micromotion.com>, Daniel® <http://www.daniel.com>, Westinghouse Process Control <http://www.westinghousepc.com>, PlantWeb® <http://www.plantweb.com>, DeltaV <http://www.easydeltav.com> and AMS <http://www.emersonprocess.com/ams>.

Abduralum,

Per our conversation this morning I think it has been made clear that the purge near the instrument will only be utilized as a manual blowback – not constant – – impact on instrument accuracy is not an issue, Refer to diagram below.

David

REACTOR IMPROVEMENT LEVEL CONTROL



-----Original Message-----

From: GHAMDI AL-, Abdulrahman A
Sent: Saturday, August 28, 2004 12:06 AM
To: LABORDE, David M; THAWADI AL-, Ahmed Y; QAHTANI AL-, Abdullah H; FAIFI AL-, Mohammed Masoud; HAGRY AL-, Ershaid M; JAZAIRI AL-, Tawfiq Mohammed
Cc: WADAEY AL-, Mohammad Z; ZHRANI AL-, Matar A; REFAEE, Ibrahim Mohammed; QAHTANI AL-, Mushabeb Z; SAIF BIN, Abdulaziz A
Subject: RE: Reactor Instrument Taps & Frequent Plugging

Ibrahim/ David

1. Install the Purge Near the instrument to keep the leads swept clean:
General practice is that the transmitter should not be purged thro the instrument for better accuracy and stability of the measurement. But we agree with you and recommend to install the purge between the transmitter and process tapping which is acceptable and valid considering the process nature.

2. Relocate the transmitter and re engineer the impulse lines with less bends:
this is also a very good suggestion to improve the performance of the measurement loop. lat us have a team to study this issue in more detail and have final recommendation.

Thanks

REACTOR IMPROVEMENT LEVEL CONTROL

Abdulrahman Al-Ghamdi
Senior.Instrument & PLC Engr.
Al-Jubail Petrochemical Co. (KEMYA)
Phone: 03 357 6539
Fax: 03 357 6058
mobile 055911014
E-mail: <mailto:ghamdiala2@kemya.sabich.com>

-----Original Message-----

From: LABORDE, David M
Sent: Sunday, May 30, 2004 2:41 PM
To: THAWADI AL-, Ahmed Y; QAHTANI AL-, Abdullah H; FAIFI AL-, Mohammed Masoud; HAGRY AL-, Ershaid M
Cc: WADAEY AL-, Mohammad Z; ZAHRANI AL-, Matar A; REFAEE, Ibrahim Mohammed; QAHTANI AL-, Mushabeb Z; GHAMDI AL-, Abdulrahman A
Subject: Reactor Instrument Taps & Frequent Plugging

Gents,

Today, Ibrahim and myself made a cursory inspection (outside) and review of existing designs for purge to the reactor instruments (nozzles). We found that the existing instruments (with purged taps) are not adequate. It appears that over time the existing instrument leads have been modified, relocated and/or re-tubed with numerous bends / dents and direction changes. The ethylene purge is also located very close the nozzle. The distance between the entry point of the purge and the actual instrument lead is very long (leaving large unpurged pocket). Pressure fluctuations in the C2 purge header and/or reactor can allow resin fines to travel (intermittently) backwards in the tubing pass the purge point (see sketch below). When this happens, the tubing becomes partially fouled and errors are seen in the Dp signals. Fluctuations in pressure during manual blowback often dislodge the material and it eventually makes it way to the purged portion of the tubing and flows back in to the reactor. Often this material remains lodged in the tubing leads and the taps must be vented or drilled.

<< OLE Object: Picture (Metafile) >>

REACTOR IMPROVEMENT LEVEL CONTROL

The solution is to install purges near the instrument to keep the leads swept clean. The existing purge lines that go directly to the nozzle can be left in tact but manually blocked. When drilling or excessive purge is required, the existing manual block can then be utilized (opened). The concept & design is shown in the sketch below. (see other recommendations below sketch).

<< OLE Object: Picture (Metafile) >>

Many of the Dp leads are very long on one side and very short on the other. I suggest we re-locate the instrument Dp cell at mid-point to equalize the leads. The existing leads (tubing) is also in poor conditions (many dents and bends). I suggest we re-tube **all leads** and relocate. All tubing "runs" should be very straight and when bends are required (minimized to as few as possible). New orifices should be sized for each purge to insure 1.8 m/s velocity at the entry point of the nozzle. All purges should be as close to the instrument as possible. I suggest we run new tubing and insure proper amounts are provided for optimum location of each instrument (to avoid tubing length and bends). These could be capped (to avoid contamination) and ready for tie-in any time the reactor is down. I believe 99% of our tap plugging problems can be attributed to the designs & conditions noted above. Every effort should be made to quickly fabricate tubing to correct errors. Ibrahim has the specifics for all of this and can be consulted for this quick improvement project.

David

Dear Mr. George

We had conference call yesterday regarding the above subject . You requested me for more detail about our process reactor . please find the attached file regarding to this issue . your feedback highly appreciated .

Thanks



10-A1-400A.pdf



10-A1-400B.pdf



Process
overview.doc

REACTOR IMPROVEMENT LEVEL CONTROL

Abdulrahman Al-Ghamdi

Our ref KC0413842

Thank you for the details.

I do not see any existing sight glass on the vessel. You may need a new nozzle in the pressure vessel.

Please state where the view of the level can be made and which, if any, nozzle can be used.

Linda: Please put a copy in the sales file.

Best regards

George Heyes

Regional Sales Office

KC Controls Ltd

2nd Floor

The Portergate

Ecclesall Road

Sheffield S11 8NX

Off tell# 01142 096203